A Comparative Sustainability Study for Treatment of Domestic Wastewater: Conventional Concrete and Steel Technology vs. Vegetated Sand Beds (VSB’s) and Their Relative Differences in CO2 Production

Alicia M. Milch
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A COMPARATIVE SUSTAINABILITY STUDY FOR TREATMENT OF DOMESTIC WASTEWATER:
CONVENTIONAL CONCRETE AND STEEL TECHNOLOGY VS. VEGETATED SAND BEDs (VSBs) AND THEIR
RELATIVE DIFFERENCES IN CO₂ PRODUCTION

A Thesis Presented
by
ALICIA M. MILCH

Submitted to the Graduate School of the
University of Massachusetts Amherst in partial fulfillment
Of the requirements for the degree of

MASTER OF SCIENCE

May, 2016

Department of Plant and Soil Sciences
A COMPARATIVE SUSTAINABILITY STUDY FOR TREATMENT OF DOMESTIC WASTEWATER:
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A final thank you goes out to my husband, parents, and friends who have supported me in various ways throughout this journey.
ABSTRACT

A COMPARATIVE SUSTAINABILITY STUDY FOR TREATMENT OF DOMESTIC WASTEWATER: CONVENTIONAL CONCRETE AND STEEL TECHNOLOGY VS. VEGETATED SAND BEDs (VSBs) AND THEIR RELATIVE DIFFERENCES IN CO\textsubscript{2} PRODUCTION

MAY 2016

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M.S., UNIVERSITY OF MASSACHUSETTS AMHERST

Directed by Dr. Ron Lavigne

Conventional wastewater treatment in the U.S. is an energy dependent and carbon dioxide emitting process. Typical mechanical systems consume copious amounts of energy, which is most commonly produced from fossil fuel combustion that results in the production of CO\textsubscript{2}. The associated organic load is also metabolized by microorganisms into CO\textsubscript{2} and H\textsubscript{2}O. As the desire to reduce CO\textsubscript{2} output becomes more prominent, it is logical to assess the costs of conventional treatment methods and to compare them to alternative, more sustainable technology. Vegetated Sand Bed (VSB) and Reed Bed (RB) systems are green technologies that provide environmentally superior treatment to conventional systems at a fraction of the cost both environmentally and economically. Using mass balance equations the net CO\textsubscript{2} produced from wastewater treatment at 3 conventional facilities, (Amherst, MA, Ithaca, NY and Shelburne-Buckland, MA) and 3 VSBs, (Lloyd, NY, Shushufindi Slaughterhouse, Ecuador and Shushufindi Municipal Facility, Ecuador), will be estimated. Carbon dioxide sources considered are BOD\textsubscript{5} microbial respiration, power demand, and sludge treatment. Using the BOD\textsubscript{5} reduction and the average daily flow from each of the conventional facilities, hypothetical VSB and RB systems will be sized for the 3 conventional systems. The land area for each hypothetical VSB and RB and the CO\textsubscript{2} reduction for equal treatment are estimated for each conventional facility. Estimates of annual CO\textsubscript{2} production for Amherst, Ithaca, and Shelburne-Buckland, are 3,021 metric tons, 5,575 metric tons, and 158 metric tons of, respectively. The annual CO\textsubscript{2} reduction potential for the conventional facilities Amherst, Ithaca, and Shelburne-Buckland, when compared to VSB and RB technology is estimated to be 74.0%, 83.2%, and 86.3% respectively. VSB and RB technology also provide promising results for sustainable wastewater treatment and reuse. Ammonium and nitrate reduction at the Joseph Troll Turf Plot VSBs were 72% and 88% respectively. The mean ammonium microbial growth rate constant was −0.14 d\textsuperscript{-1} and the mean nitrate microbial growth rate constant was −0.23 d\textsuperscript{-1}. The implications are ammonium and nitrate reduction is possible with VSB and RB technology. Further
investigation to understand the processes and fate of nitrogen including separate testing of ammonium and nitrate reduction are recommended.
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CHAPTER 1
INTRODUCTION

Due to increasing environmental damage to waterways of the U.S. prior to 1971, mounting concern and increasing political pressure led to the passing of the Federal Water Pollution Control Act Amendment of 1972 (PBS 2002). Also called the Clean Water Act (CWA 1972), it was the first amendment pertaining to wastewater discharge in the United States of America, (EPA 2007). The primary purpose of the CWA was “to make rivers and lakes fishable and swimmable” (CWA 1972), which established a foundation for regulating wastewater discharge into rivers (EPA 2007). Failing to foresee the long-term environmental and economic costs of conventional treatment and with little attention to public health, the discharge limit was and still is typically set at 30mg/L of BOD$_5$ and 30mg/L of SS to ensure sufficient oxygen in the water for fish and adequate clarity for swimming (EPA 2014). The CWA made it illegal to discharge wastewater into navigable waters from a point source without a permit (EPA 2014) so the National Pollutant Discharge Elimination System (NPDES) permit program was established to regulate the release of pollutants (EPA 2007).

According to the U. S. Environmental Protection Agency (EPA) over 75% of the current 320 million people in the US are served by centralized wastewater collection and treatment systems (EPA 2007). The United States Geological Survey (USGS) estimates that the average person uses 100 gallons of potable water per day which results in 24 billion gallons of sewage per day or $9.1 \times 10^7$ m$^3$ per day entering the municipal wastewater treatment plants across the country. The wastewater treatment at these conventional concrete and steel facilities most often relies on constant mechanical aeration powered by electricity produced primarily from fossil fuel combustion. The greatest demand for energy at a conventional wastewater treatment plant is due to the continuous aeration necessary for biological treatment ranging from 40% to 60% of the total plants energy demand (EPRI 2002).
Another environmental impact comes from the organic constituents in sewage which are broken down into the greenhouse gas carbon dioxide (CO₂) and H₂O using O₂ for the aerobic oxidation process. This indicates that with the increasing amount of wastewater entering treatment facilities, more CO₂ will be emitted into the atmosphere each year. The objective of this research is to investigate the sustainability of conventional wastewater treatment technology compared to Vegetated Sand Bed (VSB) and Reed Bed (RB) technology from a water reuse, CO₂ production, and energy consumption standpoint. For each conventional facility, a hypothetical VSB and RB system capable of receiving the same average daily flow and reducing the same concentration of BOD₅ will be postulated. The primary focus will be on total CO₂ production compiling the three major contributing sources: biological breakdown of wastewater, fossil fuel demands of operating the systems, and CO₂ produced from sludge processing.

The limitations of conventional technology for treating nutrients and complex organics like estrogen, antibiotics, and other pharmaceuticals and personal care products (PPCPs) have also become an international concern (CSS 2013). The new VSB treatment facility built and made operational in 2015 at the UMASS Turf Plots will be briefly discussed along with early influent and effluent nutrient data that will be used to model the kinetics of first order microbial decay for NH₄⁺ and NO₃⁻.

1.1 Wastewater Treatment Technology Overview

1.1.1 Conventional Technology

The most common wastewater treatment methods in the United States today utilizes concrete and steel systems designed to achieve improvement in the quality of wastewater (World Bank Group 2014). Primary treatment involves the partial physical separation of the liquids and suspended solids, ranging from rags on the collection screens to fats and sludge collected in the primary clarifier through sedimentation and flotation (EPA 2007). Secondary treatment involves the biological degradation of
the dissolved organic matter in the wastewater converting it into new bacteria cells, carbon dioxide, and other by-products (EPA 2007). In the USA, **activated sludge** (AS) is the most commonly used conventional treatment particularly for new plants larger than 1 million gallons per day (MGD) (Pabi et al. 2013). This technology uses aeration and mixing to provide oxygen for the bacteria, fungi, and protozoa that metabolize the organic matter through respiration (NESC 2003). The aeration and mixing requirements of secondary treatment are noted as the single largest energy users in AS treatment plants (Carlson and Walberger 2007). Discharge from these facilities is typically directly into rivers that run into the ocean changing the partially treated fresh wastewater effluent into salt water.

### 1.1.2 Conventional Sludge Treatment

Conventional sludge treatment can involve various mechanisms to process solids and therefore can account for up to one third of overall plant energy use, (Pabi et al. 2013). Sludge processing and the formation of biosolids as outlined by the United Nations Environment Program (UNEP) involves thickening, stabilization, and dewatering of the sludge before it can be disposed of most commonly by landfilling, land application, or incineration (2000). After wastewater treatment, sludge represents about 5% of the overall plant flow and contains about 2% dry solids, (Pabi et al. 2013). Thickening of sludge is often accomplished by gravity belts, centrifuges, or dissolved air flotation, all of which are energy consumers (Pabi et al. 2013). Stabilization is often accomplished by anaerobic or aerobic digestion but can also be accomplished by composting, (Pabi et al. 2013). A common mechanism for dewatering is by belt filter press and can achieve approximately 25%-35% solids, (Pabi et al. 2013). Dewatered sludge greater than 20% solids may be disposed of by landfilling. Alternatives to landfilling include incineration and land application (EPA 2006). Figure 1 shows the treatment steps in typical conventional activates sludge treatment.
Conventional wastewater treatment facilities may not use all of the processes from Figure 1 or may include additional processes.

**1.1.3 Vegetated Sand Bed (VSB) Technology**

Conventional wastewater treatment is currently the most commonly used method in the United States however this study explores green technology. Vegetated Sand Beds (VSBs) are manmade treatment systems designed to emulate the biological capability of natural wetland processes to break down and remove contaminants from wastewater (R. Lavigne and K. Gloger 2008). A vertical sub-surface flow VSB receives wastewater distributed over the total area of the sand bed. The wastewater moves vertically through the beds where it is metabolized by communities of bacteria that have accumulated on the media. Similar to AS treatment this technology relies on the respiration of bacteria, fungi, and protozoa to metabolize the contaminants in the wastewater however, it has several characteristics which make it a more sustainable system. Higher surface area on the media in VSB systems allow the establishment of attached growth microbes which strengthens treatment. The vegetation planted in VSBs is facultative wetland species which transport oxygen from the atmosphere.
into the root zone eliminates the need for mechanical aeration (James Hairston 2001). Figure 2 illustrates the flow of wastewater in a top fed vertical flow sub-surface Vegetated Sand Bed. Discharge from VSB’s can occur through evapotranspiration, infiltration, irrigation, or reuse of the treated water. These mechanisms allow for treated water to re-enter the water cycle as well as recharge the groundwater table which is being depleted by anthropogenic activity in many parts of the world.

**Figure 2. TOP-FED VERTICAL FLOW SUBSURFACE VEGETATED SAND BED CROSS-SECTIONAL AREA**

Vegetated Sand Beds typically function in parallel trains or in a series with wastewater passing through two or more beds. Figure 3 illustrates a typical vertical flow sub-surface VSB system.

**Figure 3. VEGETATED SAND BED SYSTEM** (Adapted from Lavigne and Spokas 2008)
Figure 4 shows the processes of wastewater treatment when using VSB and RB technology as well as the fate of the water.

**Vegetated Sand Bed (VSB) Technology with Reed Bed Dewatering Technology**

1.1.4 Reed Bed (RB) Technology

Reed Beds are a natural alternative sludge management technology that dewater, decomposes, and stabilizes sludge through drainage, evapotranspiration, plant uptake, and microbial degradation (Uggetti et al. 2012). A large portion of the energy used with conventional sludge treatment is aimed at reducing the water content. Reed Beds receiving sludge with 2% solids can eliminate approximately 95% of the water at a greatly lower cost. Over the course of 15+ years, an accumulative application of up to 130 feet of sludge reduces to 5 feet of dry biosolids in a Reed Bed system. Reed Beds are lined basins with a gravel and sand drainage network planted with Phragmites australis. They require no sludge removal between applications (Uggetti et al. 2011). Approximately 4” of sludge is applied to the Reed Bed every two weeks and dewater as the liquid percolates through the media. The reeds transport oxygen to the rhizosphere aerating and enhancing the microbial breakdown (Brix et al. 1994).
Similar to the VSBs, the Reed Beds require minimal energy input and maintenance. This technology replaces the steps required for sludge thickening, conditioning with polymers, dewatering, and frequent disposal which lowers the overall cost of sludge management (Kim and Smith 1997). Figure 5 illustrates the cross-sectional view of Reed Bed technology and how it dewateres, stores, and composts sludge over time (A. Krueger 1991).

**Figure 5. SLUDGE DEWATERING AND ACCUMULATION WITH REED BED TECHNOLOGY**

(Adapted from A. Krueger (1991) Beds: A Low-Cost Sludge Treatment System)
1.2 Vegetated Sand Bed Processes

1.2.1 Biochemical Oxygen Demand Removal

The removal of BOD$_5$ in a subsurface-flow VSB is enhanced by the aerobic and anaerobic microbial interactions that facilitate a variety of metabolic pathways for attached growth organisms. The solid media in the Vegetated Sand Bed provides a large fixed surface area where organisms can build up populations that are not flushed through the system. Coarse sand with a diameter of 2 mm has the surface area of approximately $10^{-3}$ m$^2$/cm$^3$, (G. Hirasaki 2004), which translates to 1000 m$^2$/m$^3$ surface area in addition to any root surfaces present. A comparable volume in free-water-surface wetland might have 15-50 m$^2$/m$^3$ available surface area, (Reed et al. 1995).

The size of the aerobic and anaerobic zones in a VSB fluctuate due to multiple conditions and plays an important role in the type of treatment accomplished. Oxygen gas is pumped by the facultative wetland plants to the root zone where the excess diffuses into the VSB media (Spokas and Lavigne 2008). An oxic annulus is created around the roots which results in a zone of aerobic biological and chemical processes such as the oxidation of carbon and nitrogen (Kahl 2004). Figure 6 shows the cross sectional area of a root found in a VSB. The size of the annulus is determined by the demand of oxygen from aerobic processes as well as the plants’ ability to provide oxygen to the roots. Influent wastewater with high concentrations of BOD$_5$ can result in bacteria using available O$_2$ at faster rates and therefore can cause the oxygen annulus around the roots to decrease. An additional source of oxygen in the VSB system is found in top-loading vertical flow VSBs where the suction created by percolation water, draws oxygen into the subsurface of the system.
Figure 6. CROSS-SECTION OF WETLAND ROOT ANNULUS
Dynamics of root-growth media interface (Adapted from Reed et al. 1995).

Figure 7 illustrates a side view of the distribution of oxygen in the root zone of a VSB or RB.

New plants will have minimal root systems and overloading the system with high concentrations of BOD5 or ammonium could deplete the oxygen levels and stress the plants. The operation of a VSB must be monitored to maintain the quantity of oxygen needed to support the aerobic treatment processes and to provide oxygen needed for the growth of the vegetation.
The distribution of oxic and anoxic zones is not solely a function of depth. The oxygen distribution found in VSBs and RBs is dependent on the depth and extensiveness of the root system.
1.2.2 Kinetics of VSB Design

The desired treatment time in a VSB system is typically calculated using a first order decay model for \( BOD_5 \) reduction (Kahl 2004) see equation [1].

\[
\frac{dC}{dt} = -k \cdot C \quad [1]
\]

Where \( C \)= the concentration of \( BOD_5 \) remaining in mg/L

\( t \)= treatment time in days

\( k \)= typical domestic sewage first order decay rate constant 1.2 days\(^{-1}\) for temperate climates and 1.5 days\(^{-1}\) in tropical climates

The first order decay rate constant can be adjusted for different ambient temperatures using equation [2].

\[
\frac{k_T}{k_{20}} = 1.06^{T-20} \quad [2]
\]

After separating the variables \( C \) and \( t \) and integrating, equation [1] can be expressed in terms of concentration or time shown in equation [3] and equation [4].

\[
C_t = C_0 \times e^{-k \cdot t} \quad [3]
\]

\[
t = \frac{1}{k} \ln \left( \frac{C_0}{C_t} \right) \quad [4]
\]

Where \( C_0 \)= initial concentration of \( BOD_5 \) (mg/L)

\( C_t \)= concentration of \( BOD_5 \) at time \( t \) (mg/L)
Once the required treatment time is calculated using initial and desired effluent concentration, the size of the wetland can be calculated using equation [5].

\[ Q = \frac{A \cdot h \cdot f}{t} \quad [5] \]

Where \( Q \) = daily flow rate (volume/time)

\( t \) = treatment time in days (t)

\( A \) = wetland area (L^2)

\( h \) = wetland depth, (L)

\( f \) = porosity of media (dimensionless)
CHAPTER 2
MATERIALS AND METHODS

Most wastewater systems receive influent with organic matter in the form of proteins, carbohydrates, and fats which are the biomass produced from photosynthetic activity. For the following mass balance, the BOD₅ in the wastewater will be represented as glucose because it and the organics have a basic stoichiometric relationship. The fats, carbohydrates, and proteins in BOD₅ are expressed as glucose in equation [6].

\[ C_6H_{12}O_6 + 6O_2 \rightarrow 6CO_2 + 6H_2O \quad [6] \]

This equation stoichiometrically converted to kilograms, provides a foundation with which the amount of CO₂ sequestered and released can be approximated. Using changes in the BOD₅ influent and effluent, the amount of organic matter respired during treatment can be estimated. Equation [7] predicts the amount of CO₂ produced.

\[ 180kg \ C_6H_{12}O_6 + 192kg \ O_2 \leftrightarrow 264kg \ CO_2 + 108kg \ H_2O \quad (\text{Lavigne and Gloger, 2008}) \quad [7] \]

Example Calculations:

Assuming raw wastewater BOD₅ of 200mg/L and desired effluent BOD₅ of 25mg/L

BOD₅ removal = 175 mg/L = 0.175kg/m³

Applying this reduction to the total U.S. sewage production of 9.1x10⁷ m³/day, 1.7x10⁷ kgBOD₅/day are biodegraded to CO₂ and water.

Using equation [7], the CO₂ emissions from microbial respiration is 25 million kg CO₂/day.
2.1 Conventional Wastewater Treatment Sites-Three Case Studies

2.1.1 Amherst Wastewater Treatment Plant, MA

The Amherst Wastewater Treatment Plant (AWWTP) processes the municipal wastewater from the Town of Amherst and the University of Massachusetts. The facility uses activated sludge (AS) to accomplish secondary treatment. The technology is powered by continual aeration and electric pumps move the wastewater to the various stages and locations. The plant receives an average daily flow of 3.85MGD with a peak of 8.54MGD in 2014. The final treatment step is chlorination that occurs in the
pipe that discharges the effluent into the Connecticut River (AWWTP 2014). Sludge management at the Amherst Wastewater Treatment facility is a multiple step process. Sludge from the primary clarifier is combined with sludge from the secondary clarifiers with an average 4% solid before it is sent to the gravity belt thickener where it is partially dewatered. The Thickened Waste Activated Sludge (TWAS) has 6% solids and it is stored until pumped into tanker trucks and transported to Hartford landfill in Connecticut. In Hartford it is dewatered, incinerated, and landfilled. The AWWTF produces approximately 4.2MG/year of sludge with 6% solids.
2.1.2 Ithaca Area Wastewater Treatment Facility, NY

The Ithaca Area Wastewater Treatment Facility (IAWWTF) treats residential wastewater from the city, two universities, and industrial waste from Emerson Power Transmission Company. The average daily flow is 6.5MGD (Wastewater Treatment Ithaca 2006). Secondary treatment is accomplished by activated sludge with four aeration basins operating in a plug-flow mode, each having 0.5 MG of volume and a fine bubble diffuser system. Disinfection occurs in the pipe that discharges the effluent into Cayuga Lake which is part of the Great Lakes Basin, (MWWT 2005). Primary and secondary sludge are combined and pumped to two gravity thickeners. The sludge with an average of 4% solids is pumped to a belt filter press that operates five days per week. The dewatered sludge leaves the facility at about 22% solids and the sludge cake is landfilled, (NYSERDA 2005).
2.1.3 Shelburne-Buckland Wastewater Treatment Plant, MA

The Shelburne-Buckland Wastewater Treatment Plant was constructed in 1974 to serve two densely populated business districts. The facility uses activated sludge treatment with aerobic sludge digestion and was built with a maximum capacity of 0.25MGD. On average this wastewater treatment plant processes 0.144MGD (J. S. Begg et al. 2001), and the effluent is discharged into the Deerfield River. Sludge management originally utilized sand drying beds followed by trucking of the cake to the town landfill. Limitations with the sand drying beds included solids washing out during rain events, limited sludge storage in the digester, (approximately 52,000 gallons or 6 weeks), and the inability to dewater during the winter, (D. Fleuriel 2008). In 1984 a sludge storage lagoon was constructed but due to an
inadequately sized surface aerator, the sludge lagoon went anaerobic causing significant odor problems. Alternative solutions were attempted by renting a belt filter press for dewatering during winter months, but costs remained high and odor problems continued. Finally, in 1992 the decision was made to convert the sludge management program to Reed Bed Technology.

By 1995, the Shelburne-Buckland wastewater treatment plant had three operational Reed Beds with a total surface area of 12,000 square feet. The beds dose on a 3 week schedule receiving approximately 25,000 gallons per dose and 450,000 gallons per year with 1.5% solids. Over the course of a 6 year study, the dewatering efficiency of the Reed Bed system was determined to be 93% (J.S. Begg et al. 2001). The average BOD₅ effluent concentrations leaving the Reed Bed systems were found to normally be around 6mg/L which is well below regulatory standards and therefore could be discharged directly into the river (J.S. Begg et al. 2001). Electrical demands for the plant include pumping sewage from the two villages, recirculating the wastewater, and aeration in the aeration tanks and digester (D. Fleuriel 2008). The only waste removed from the site is grit and screenings collected at the head works.
2.2 Vegetated Sand Bed Technology

Photo 6 Lloyd Vegetated Sand Beds (Courtesy of NEWS-USA 2006)

2.2.1 Zumtobel Staff Lighting VSB Lloyd, NY

Zumtobel Staff Lighting is located in the Town of Lloyd NY, and is one of the largest employers in the area. In 2000, their conventional septic system went into failure and the company seemed to have only two options: connect to the nearest sewer line for 3 million dollars or to replace the mound system using an area previously dedicated for the future expansion of the company. Another alternative solution was to relocate the company to New Jersey. Before a decision was made, the sewer and water commissioner, John Jankiewicz proposed the implementation of a Vegetated Sand Bed; a sustainable green plant-powered alternative technology that decentralizes wastewater treatment. Considering the
costs of connecting to the municipal AS treatment system, the loss of local jobs, and the expansion of the company versus the benefits of a VSB for wastewater treatment, the failing septic system in Highland NY went green.

The Lloyd VSB design consists of four treatment cells in series with each bed constructed at 2,500 ft² for a total area of 10,000ft². The septic tank effluent has wastewater first passing through the two beds planted with *Phalaris arundinacea*, commonly known as Reed Canary Grass and then through two beds planted with *Phragmites communis*. The design flow rate was 10,000 GPD with an average daily flow of 1,200 GPD in 2005. The system was oversized at 400% to facilitate possible future connections from other wastewater sources in the area (Lavigne and Spokas 2009). The effluent is discharged to a small pond (Kahl 2004).

2.2.2 Shushufindi, Ecuador, S.A.

Shushufindi is a town in Ecuador, South America, at the headwaters of the Amazon River. Due to the expansion of the oil industry, the population of Shushufindi has grown rapidly over the years. This development has led to degradation in the environment of the town and consequently other settlements down river. To compensate for the continual increase of wastewater that received little to no treatment, Texaco donated money to build a sewage collection system in 1997. After assessing the total cost, longevity, and treatment quality, the wastewater management technology selected for use was Vegetated Sand Beds. The first system was implemented at the town slaughterhouse, where previously the facility discharged its untreated wastewater directly into the Rio Shushufindi (Kahl 2004).
2.2.2.1 Shushufindi Slaughterhouse VSB, Ecuador

The VSB system at the slaughterhouse was designed to treat 6,600 gallons/day or 25 m$^3$/d of slaughtered animal wash water. The influent primarily consists of blood, urine, feces, and undigested plant material making it a high BOD$_5$ and suspended solids wastewater. After passing through two settling tanks in series with a total volume of about 10,000 gallons or 38 m$^3$, the wastewater passes through two wetland cells also operated in series, with an area of 8,600 ft$^2$ or 800 m$^2$. The treatment cells are planted with a local wetland plant *Echinochloa polystachya*, or commonly known as German Grass. The grass has a primary productivity of 4 kg/m$^2$/yr (Kahl 2004). The VSBs require minimal maintenance because they were designed to operate by gravity. The system does not use any electricity (Kahl 2004).
2.2.2.2 Shushufindi Municipal VSB, Ecuador

The Shushufindi Municipal VSBs were designed to treat 0.53 MGD or 2000 m$^3$/d of municipal wastewater. Four 13,200 gallon or 250 m$^3$ settling tanks start the treatment and connect to four parallel treatment trains. Each train has two VSBs with a total of 8 units each unit being 21,500 ft$^2$ or 2,000 m$^2$. Similar to the VSB at the Shushufindi slaughterhouse treatment units operate by gravitational flow and they are planted with German Grass. The Shushufindi Municipal VSB also has 4 Reed Beds located adjacent to the settling tanks that are used to dewater the sludge (Kahl 2004).
CHAPTER 3
COMPARATIVE DATA

The objective of this study was to compare the sustainability of conventional wastewater treatment systems to Vegetated Sand Bed and Reed Bed technology. In order to accomplish such a comparison, it was necessary to categorize and group the most critical impacts of wastewater treatment which include the fate of fresh water, CO₂ production, and energy consumption. Energy consumption and the production of carbon dioxide will be compared by estimating the metric tons of CO₂ produced from BOD₅ microbial respiration and power demand at each facility.

3.1 Current Treatment

3.1.1 Amherst Wastewater Treatment Plant, MA

3.1.1.1 Biochemical Oxygen Demand

The average flow in 2015 was 3.51 million gallons per day (MGD) and it was the lowest flow of 2012, 2013, 2014, and 2015. Figure 8 illustrates the average daily flow to Amherst WWTP from 2012 to 2015.
The wastewater at Amherst enters the plant with an average 227mg/L of BOD$_5$ and typically leaves at 2mg/L resulting in an average 99% removal rate for 2015. Figure 9 presents the influent and effluent BOD$_5$ values at Amherst WWTP from 2012-2015. The change in influent BOD$_5$ and effluent BOD$_5$ can easily be compared to determine the amount of BOD$_5$ removed.
Figure 9. AVERAGE INFLUENT AND EFLLUENT BOD$_5$ AT AMHERST WWTP 2012-2015.

Table 1 provides values for average daily flow, influent BOD$_5$, and effluent BOD$_5$ per day and per year from 2012-2015. Data was obtained from Amherst Wastewater Treatment Plant.

Table 1. AVERAGE DAILY FLOW, INFLUENT BOD$_5$, AND EFFLUENT BOD$_5$

<table>
<thead>
<tr>
<th>Amherst WWTP</th>
<th>2012</th>
<th>2013</th>
<th>2014</th>
<th>2015</th>
</tr>
</thead>
<tbody>
<tr>
<td>Year</td>
<td>Average Flow (MGD)</td>
<td>Influent BOD$_5$ (mg/L)</td>
<td>Effluent BOD$_5$ (mg/L)</td>
<td></td>
</tr>
<tr>
<td>2012</td>
<td>4.55</td>
<td>184</td>
<td>3.25</td>
<td></td>
</tr>
<tr>
<td>2013</td>
<td>4.11</td>
<td>190</td>
<td>3.25</td>
<td></td>
</tr>
<tr>
<td>2014</td>
<td>3.85</td>
<td>166</td>
<td>2.14</td>
<td></td>
</tr>
<tr>
<td>2015</td>
<td>3.51</td>
<td>227</td>
<td>2.00</td>
<td></td>
</tr>
</tbody>
</table>

Provided data from AWWTP manipulated to show average flow, BOD$_5$ influent and effluent per day.
3.1.1.2 Carbon Dioxide

The carbon dioxide produced from BOD₅ degradation at the Amherst Wastewater Treatment Facility was calculated using the average daily flow. The average BOD₅ microbial respiration in mg/L was calculated per day using the values from Table 1. Multiplying the average BOD₅ removal concentration by the average daily flow, the total BOD₅ in kilograms removed per day was calculated. Estimating CO₂ produced from the average BOD₅ reduction is calculated by applying equation [7] which stoichiometrically expresses the relationship between BOD₅, represented as glucose, and CO₂ production. Table 2 presents the calculated values.

In 2015, the average influent BOD₅ was 227mg/L and the effluent BOD₅ was 2mg/L

\[
\text{BOD₅ removal} = 225 \text{ mg/L }= 0.225 \text{ kg/m}^3
\]

\[
0.225 \frac{kg}{m^3} \cdot \frac{1m^3}{264 \text{ gal.}} = 8.52 \times 10^{-4} \text{ kg of BOD₅ per gallon}
\]

Average Flow of 3.51MGD

\[
3,510,000 \frac{\text{gallons}}{\text{day}} \cdot 8.53 \times 10^{-4} \frac{\text{kg BOD₅}}{\text{gallon}} = 2,990 \text{ kg BOD₅ per day}
\]

Using equation [7], CO₂ emissions from microbial respiration, 1.47 kg of CO₂ is produced for every 1 kg of C₆H₁₂O₆, (represented by BOD₅).

\[
180\text{kg } C_6H_{12}O_6 + 192\text{kg } O_2 \leftrightarrow 264\text{kg } CO_2 + 108\text{kg } H_2O \quad [7]
\]

\[
2,990 \text{ kg BOD₅ per day } \times 1.47 \text{ kg CO₂/1 kg BOD₅}
\]

Estimated CO₂ production from microbial respiration is 4,400 kg/day or 1,600,000 kg/year.
TABLE 2. AVERAGE BOD$_5$ REMOVAL AND ESTIMATED CO$_2$ PRODUCED

<table>
<thead>
<tr>
<th>Amherst WWTP</th>
<th>2012</th>
<th>2013</th>
<th>2014</th>
<th>2015</th>
</tr>
</thead>
<tbody>
<tr>
<td>Year</td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Average Flow (MGD)</td>
<td>4.55</td>
<td>4.11</td>
<td>3.85</td>
<td>3.51</td>
</tr>
<tr>
<td>BOD$_5$ Removed (mg/L)</td>
<td>181</td>
<td>187</td>
<td>164</td>
<td>225</td>
</tr>
<tr>
<td>Average BOD$_5$ total (kg/day)</td>
<td>3,120</td>
<td>2,910</td>
<td>2,390</td>
<td>2,990</td>
</tr>
<tr>
<td>Average CO$_2$ Produced (kg/day)</td>
<td>4,590</td>
<td>4,280</td>
<td>3,520</td>
<td>4,400</td>
</tr>
<tr>
<td>Average CO$_2$ Produced (kg/year)</td>
<td>1,680,000</td>
<td>1,560,000</td>
<td>1,280,000</td>
<td>1,600,000</td>
</tr>
</tbody>
</table>

Flow and BOD$_5$ data was obtained from Amherst Wastewater Treatment Plant.

The average daily flow to Amherst WWTP has continually decreased from 2012-2015. Figure 10 plots the relationship between CO$_2$ production and average daily flow from 2012-2015. It is clear that the CO$_2$ produced from the biological processes in wastewater treatment is influenced by both the flow of the plant and by the BOD$_5$ metabolized.
Figure 10. AVERAGE DAILY FLOW AND AVERAGE CO₂ PRODUCED AT AMHERST WWTP

Flow data from Amherst Wastewater Treatment Plant. Provided average daily flows from AWWTP plotted against estimated kilograms of CO₂ produced from microbial respiration of BOD₅.

3.1.1.3 Power Demand

The electric meter at the Amherst Wastewater Treatment Facility includes all onsite power usage from lights, pumping, and aeration. Not included in these figures are the power demands from the 20 pumping stations located across Amherst and the sludge transport and incineration costs in Hartford, CT. Figure 11 presents the relationship between the average flow and the electrical demand used for treatment. The electrical demand per MGD treated increased over the past three years. Figure 11 suggests that an increase of BOD₅ microbial respiration in conventional facilities can result in greater energy demands per MGD.
Figure 11. AVERAGE DAILY FLOW COMPARED WITH AVERAGE KWH DEMAND
Flow and power data obtained from Amherst Wastewater Treatment Plant. Data provided by AWWTP shows average daily flow and average electrical demand from 2012-2015.

The Amherst Wastewater Treatment Facility reported using 1,500,000 kWh in 2015. Using the CO₂ output conversion rate, (EPA 2014), it is estimated that 1,030 metric tons of carbon dioxide was produced in 2015.

\[
6.89551 \times 10^{-4} \text{ metric tons CO}_2 / \text{kWh} \quad \text{(EPA 2014)}
\]

\[
1,500,000 \text{ kWh} \cdot 6.89551 \times 10^{-4} \text{ metric tons CO}_2 / \text{kWh} = 1,030 \text{ metric tons CO}_2 \text{ in 2015}
\]

Table 3 shows the average daily flow, annual kWh usage, kWh per MG treated, and total annual metric tons of CO₂ produced. Despite the decreasing flow from 2012-2015, the annual electrical demands increased. As shown in Table 3, the CO₂ produced per MG treated has increased from 2012-2015 at Amherst.
Table 3. AVERAGE DAILY FLOW, KWH USAGE, AND ESTIMATED CO₂ PRODUCTION

<table>
<thead>
<tr>
<th>Amherst WWTP</th>
<th>Power Demand</th>
</tr>
</thead>
<tbody>
<tr>
<td>Year</td>
<td>2012</td>
</tr>
<tr>
<td>Average Flow (MGD)</td>
<td>4.55</td>
</tr>
<tr>
<td>Annual Usage kWh</td>
<td>1,140,000</td>
</tr>
<tr>
<td>KWh/MG</td>
<td>684</td>
</tr>
<tr>
<td>Total Annual Metric tons of CO₂</td>
<td>786</td>
</tr>
</tbody>
</table>

Provided average daily flow and power demand data from Amherst WWTP 2012-2015. Calculated annual metric tons of CO₂ produced from power demand.

Figure 12 presents the calculated kWh use per million gallons treated taken from Table 3. The data shows the continual increase in kWh demand per MG from 2012-2015.

Figure 12. RELATIONSHIP OF KWH PER MILLION GALLONS OF WASTEWATER
Provided data for 2012-2015 from AWWTP.
3.1.1.4 Sludge Treatment

Sludge processing at the AWWTP is done by partial dewatering using a gravity belt thickener. The Thickened Waste Activated Sludge in its final state consists of 6% solids and is stored until it can be transported. No further electrical demands are included in the summary of the power needs for the AWWTP. In order to have a more complete account of the energy demand required to process wastewater with conventional treatment, the final sludge treatment processes were estimated.

In 2015, AWWTP sent 622 tractor trailers of liquid sludge with 6% solids to the Hartford Incinerator. According to the United States Bureau of Transportation, the average combination truck fuel consumption in 2013 was 5.8 miles/gallon. The round trip from AWWTP to the Hartford Incinerator is 106 miles.

\[
\frac{1 \text{ gallon}}{5.8 \text{ miles}} \cdot 106 \text{ miles} \cdot \frac{622 \text{ trucks}}{\text{year}} = 11,400 \text{ gallons of diesel \cdot year}^{-1}
\]

According to the US EPA, the average CO₂ emissions resulting from diesel fuel is 10.1kg of CO₂ / gallon of diesel (2005).

\[
\frac{11,400 \text{ gallons}}{\text{year}} \cdot \frac{10.1 \text{ kg}}{\text{gallon of diesel}} = 115,000 \text{ kg of CO₂/ year or 115 metric tons of CO₂/year}
\]
The final treatment is accomplished by a Nichols-Herreshoff Multiple Hearth Incinerator at the Hartford landfill in Connecticut. According to the equipment and operation permit issued by the Bureau of Air Management, this incinerator has nine hearths with a zero hearth afterburner and a Venturi-Pak scrubber as an air quality control unit, (Bureau of Air Management 2013). The maximum annual sludge charging rate is 21,060 Dry Tons (DT)/yr, and the primary fuel fired in the unit is sewage sludge. The auxiliary burner system operates on natural gas and the maximum annual fuel firing rate is 180,000 therms/year (Bureau of Air Management 2013). With this information we can calculate the approximate carbon dioxide produced during the final sludge treatment process. Table 4 shows the calculated CO₂ production estimates from Amherst sludge using known energy demands from the processes.
Table 4. PRODUCTION OF CO₂ FROM SLUDGE INCINERATION AND TRANSPORT

<table>
<thead>
<tr>
<th>Year</th>
<th>2013</th>
<th>2014</th>
<th>2015</th>
</tr>
</thead>
<tbody>
<tr>
<td>INCINERATION</td>
<td>Dry Ton Sludge/Year (DT/yr)</td>
<td>INCINERATION</td>
<td>Dry Ton Sludge/Year (DT/yr)</td>
</tr>
<tr>
<td>Amherst WWTP</td>
<td>1040</td>
<td>1000</td>
<td>1020</td>
</tr>
<tr>
<td>Hartford Incinerator (HI)</td>
<td>21,100</td>
<td>21,100</td>
<td>21,100</td>
</tr>
<tr>
<td>Percent of HI Use by AWWTP</td>
<td>4.93%</td>
<td>4.74%</td>
<td>4.83%</td>
</tr>
<tr>
<td>Natural Gas (Therms/ year)</td>
<td>88700</td>
<td>85300</td>
<td>87000</td>
</tr>
<tr>
<td>Metric Tons of CO₂/year</td>
<td>469</td>
<td>455</td>
<td>463</td>
</tr>
<tr>
<td>TRANSPORT</td>
<td>Diesel Consumption</td>
<td>TRANSPORT</td>
<td>Diesel Consumption</td>
</tr>
<tr>
<td>Amherst Trucks/ year</td>
<td>652</td>
<td>634</td>
<td>622</td>
</tr>
<tr>
<td>Gallons Consumed/ year</td>
<td>11,900</td>
<td>11,600</td>
<td>11,400</td>
</tr>
<tr>
<td>Metric Tons of CO₂/ year</td>
<td>120</td>
<td>117</td>
<td>115</td>
</tr>
<tr>
<td>Total Offsite Metric Tons CO₂</td>
<td>589</td>
<td>572</td>
<td>578</td>
</tr>
</tbody>
</table>

Provided annual sludge data from AWWTP. Estimated energy values for transport and incineration of sludge at Hartford Incinerator.

3.1.2 Ithaca Area Wastewater Treatment Facility, NY

3.1.2.1 Biochemical Oxygen Demand

The average Flow from Ithaca was 7.03 MGD in 2003. The wastewater entered the plant with an average 178mg/L of BOD₅ and left at 8.7 mg/L resulting in an average 95% removal rate. Table 5 provides values for average daily flow, influent BOD₅, and effluent BOD₅ from 2002-2003.

Table 5. AVERAGE DAILY FLOW, INFLUENT BOD₅, AND EFFLUENT BOD₅

<table>
<thead>
<tr>
<th>Ithaca AWWTF</th>
<th>2002</th>
<th>2003</th>
</tr>
</thead>
<tbody>
<tr>
<td>Year</td>
<td></td>
<td></td>
</tr>
<tr>
<td>Average Flow (MGD)</td>
<td>6.48</td>
<td>7.03</td>
</tr>
<tr>
<td>Influent BOD₅ (mg/L)</td>
<td>194</td>
<td>178</td>
</tr>
<tr>
<td>Effluent BOD₅ (mg/L)</td>
<td>14.4</td>
<td>8.7</td>
</tr>
</tbody>
</table>

Provided average flow, influent BOD₅, and effluent BOD₅ from Ithaca WWTF, (NYSERDA 2005).
3.1.2.2 Carbon Dioxide

The carbon dioxide produced by the plant was calculated from the average BOD$_5$ microbial respiration and the average daily flow. Applying the values from Table 5, the average BOD$_5$ removed per day was calculated. Using the removal concentration of BOD$_5$ and the average daily flow, the total BOD$_5$ was calculated. The CO$_2$ produced was estimated by applying equation [7]. Table 6 presents the calculated values in kilograms per day for Ithaca.

In 2003, the average influent BOD$_5$ was 178mg/L and effluent BOD$_5$ left at 8.7mg/L.

BOD$_5$ removal = 169 mg/L = 0.169kg/m$^3$

$$0.169 \frac{kg}{m^3} \cdot \frac{1m^3}{264\text{ gal.}} = 6.40 \times 10^{-4} \text{ kg of BOD}_5 \text{ per gallon}$$

Average Flow of 7.03MGD

$$7,030,000 \frac{\text{gallons}}{\text{day}} \cdot 6.40 \times 10^{-4} \frac{\text{kgBOD}_5}{\text{gallon}} = 4,500 \text{ kg BOD}_5 \text{ per day}$$

Using equation [7], CO$_2$ emissions from microbial respiration, 1.47 kg of CO$_2$ is produced for every 1 kg of C$_6$H$_{12}$O$_6$, represented by BOD$_5$.

$$180\text{ kg C}_6\text{H}_{12}\text{O}_6 + 192\text{ kg O}_2 \leftrightarrow 264\text{ kg CO}_2 + 108\text{ kg H}_2\text{O} \quad [7]$$

$$4,500 \text{ BOD}_5 \text{ /day x 1.47 kg CO}_2 / \text{ 1 kg BOD}_5$$

Estimated CO$_2$ production from microbial respiration is 6,620 kg/day or 2,410,000 kg/year.
Table 6. AVERAGE BOD₅ REMOVAL, AND ESTIMATED CO₂ PRODUCED

<table>
<thead>
<tr>
<th>Ithaca AWWTF</th>
<th></th>
<th></th>
</tr>
</thead>
<tbody>
<tr>
<td>Year</td>
<td>2002</td>
<td>2003</td>
</tr>
<tr>
<td>Average Flow (MGD)</td>
<td>6.48</td>
<td>7.03</td>
</tr>
<tr>
<td>Average BOD₅ Removal (mg/L)</td>
<td>180</td>
<td>169</td>
</tr>
<tr>
<td>Average BOD₅ total (kg/day)</td>
<td>4,420</td>
<td>4,500</td>
</tr>
<tr>
<td>Average CO₂ Produced (kg/day)</td>
<td>6,490</td>
<td>6,620</td>
</tr>
<tr>
<td>Average CO₂ Produced (kg/year)</td>
<td>2,370,000</td>
<td>2,410,000</td>
</tr>
</tbody>
</table>


3.1.2.3 Power Demand

The highest electrical demands are from the aeration system blowers, pumping systems, heating, and ventilation. The aeration during secondary treatment is done with a fine bubble diffusers, and represents 42.7% of the power demand. The processing of sludge is done by a belt filter press, reducing the water content from 94% to 78%. The belt filter press uses 0.5% of the total power demand, however, the start to finish processing of solids uses up to 10% of the total power. The cake at 22% solids is trucked to the landfill.

The Ithaca Area Wastewater Treatment Facility reported using 3,520,000 kWh in 2003. Using the CO₂ output conversion rate, (EPA 2014), it is estimated that 2,430 metric tons of carbon dioxide was produced in 2003.

\[
6.89551 \times 10^{-4} \text{ metric tons CO}_2 / \text{kWh} \quad \text{(EPA 2014)}
\]

\[
3,520,000 \text{ kWh} \times 6.89551 \times 10^{-4} \text{ metric tons CO}_2 / \text{kWh} = 2,430 \text{ metric tons CO}_2 \text{ in 2003}
\]
Table 7 summarizes the average daily flow, annual kWh usage, kWh per MG treated, and total annual metric tons of CO₂ produced. Ithaca uses natural gas for some facility power so the average annual therms, average therms/MG, and the annual metric tons of CO₂ produced from natural gas is included. The conversion rate of therms to metric tons CO₂ is applied to estimate average annual production.

\[ 0.005302 \text{ metric tons of CO}_2/\text{therm} \]  \hspace{1cm} \text{(EPA 2014)}

\[ 140,000 \text{ therms} \times 0.005302 \text{ metric tons of CO}_2/\text{therm} = 742 \text{ metric tons of CO}_2 \text{ in 2003} \]

### Table 7. AVERAGE DAILY FLOW, KWH USAGE, THERM USAGE, AND ESTIMATED CO₂ PRODUCTION

<table>
<thead>
<tr>
<th>Year</th>
<th>2002</th>
<th>2003</th>
</tr>
</thead>
<tbody>
<tr>
<td><strong>Ithaca Electricity</strong></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Flow (MGD)</td>
<td>6.48</td>
<td>7.03</td>
</tr>
<tr>
<td>Average Annual Use kWh</td>
<td>3,450,000</td>
<td>3,520,000</td>
</tr>
<tr>
<td>Average kWh/MG</td>
<td>532,000</td>
<td>501,000</td>
</tr>
<tr>
<td>Annual Metric Tons of CO₂</td>
<td>2,380</td>
<td>2,430</td>
</tr>
<tr>
<td><strong>Ithaca Natural Gas</strong></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Average Annual Therms</td>
<td>129,000</td>
<td>140,000</td>
</tr>
<tr>
<td>Average Therms/MG</td>
<td>19,900</td>
<td>19,900</td>
</tr>
<tr>
<td>Annual Metric Tons of CO₂</td>
<td>682</td>
<td>742</td>
</tr>
<tr>
<td>Total Annual Metric Tons CO₂</td>
<td>3,060</td>
<td>3,170</td>
</tr>
</tbody>
</table>

3.1.3 Shelburne-Buckland Wastewater Treatment Plant, MA

3.1.3.1 Biochemical Oxygen Demand

At the Shelburne-Buckland Wastewater Treatment Plant the recorded average flow in 2015 was 0.133 MGD. The influent BOD$_5$ was 189 mg/L and the effluent left at 4.7 mg/L resulting in a 98% removal rate. Figure 13 presents the change in average daily flow to Shelburne-Buckland WWTP from 2012-2015.

![Figure 13. AVERAGE DAILY FLOW FROM SHELBURNE-BUCKLAND WWTP 2012-2015](image)

Figure 13 shows the difference of influent and effluent BOD$_5$ since 2012. The change of total BOD$_5$ removed can also be seen in Figure 14, with the highest removal rate in 2015.
Figure 14. AVERAGE INFLUENT AND EFFlUENT BOD$_5$ AT SHELBURNE-BUCKLAND WWTP 2012-2015
Provided influent and effluent BOD$_5$ for 2012-2015 by Shelburne-Buckland WWTP.

Table 8 presents values for average flow, influent BOD$_5$, and effluent BOD$_5$ per day and per year from 2012-2015 at Shelburne-Buckland WWTP.

Table 8. AVERAGE DAILY FLOW, INFLUENT BOD$_5$, AND EFFLUENT BOD$_5$

<table>
<thead>
<tr>
<th>Shelburne-Buckland WWTP</th>
<th>Year</th>
<th>2012</th>
<th>2013</th>
<th>2014</th>
<th>2015</th>
</tr>
</thead>
<tbody>
<tr>
<td>Average Flow (MGD)</td>
<td></td>
<td>0.131</td>
<td>0.152</td>
<td>0.160</td>
<td>0.133</td>
</tr>
<tr>
<td>Influent BOD$_5$ (mg/L)</td>
<td></td>
<td>165</td>
<td>139</td>
<td>138</td>
<td>189</td>
</tr>
<tr>
<td>Effluent BOD$_5$ (mg/L)</td>
<td></td>
<td>3.3</td>
<td>2.9</td>
<td>4.4</td>
<td>4.7</td>
</tr>
</tbody>
</table>

Provided flow, influent BOD$_5$, and effluent BOD$_5$ from Shelburne-Buckland WWTP for 2012-2015.
3.1.3.2 Carbon Dioxide

The carbon dioxide produced by the BOD₅ degradation at the Shelburne-Buckland Wastewater Treatment Plant was calculated using the average daily flow. The average BOD₅ microbial respiration in mg/L was calculated per day using the values from Table 8. Multiplying the average BOD₅ removal concentration by the average daily flow, the total BOD₅ in kilograms removed per day was calculated. Estimating CO₂ produced from the average BOD₅ reduction is calculated by applying equation [7] which stoichiometrically expresses the relationship between BOD₅, represented as glucose, and CO₂ production. Table 9 presents the calculated values in kilograms per day.

In 2015, influent BOD₅ was 189mg/L and the effluent BOD₅ was 4.7mg/L

BOD₅ removed = 184 mg/L =0.184kg/m³

\[
0.184 \frac{kg}{m³} \cdot \frac{1m³}{264 \text{ gal.}} = 6.97 \times 10^{-4} \text{ kg of BOD₅ per gallon}
\]

Average Flow of 0.133 MGD

\[
133,000 \frac{\text{gallons}}{\text{day}} \cdot 6.97 \times 10^{-4} \frac{\text{kg BOD₅}}{\text{gallon}} = 92.7 \text{ kg BOD₅ per day}
\]

Using equation [7], CO₂ emissions from microbial respiration, 1.47 kg of CO₂ is produced for every 1 kg of C₆H₁₂O₆, (represented by BOD₅).

\[
180\text{kg C₆H₁₂O₆} + 192\text{kg O₂} \leftrightarrow 264\text{kg CO₂} + 108\text{kg H₂O} \quad [7]
\]

92.7 kg BOD₅/day x 1.47kg CO₂/ 1 kg BOD₅

Estimated CO₂ production from microbial respiration is 136 kg/day or 49,700 kg/year.
Table 9. AVERAGE BOD₅ REMOVAL AND ESTIMATED CO₂ PRODUCED

<table>
<thead>
<tr>
<th>Shelburne-Buckland WWTP</th>
<th>2012</th>
<th>2013</th>
<th>2014</th>
<th>2015</th>
</tr>
</thead>
<tbody>
<tr>
<td>Average Flow (MG)</td>
<td>0.131</td>
<td>0.152</td>
<td>0.160</td>
<td>0.133</td>
</tr>
<tr>
<td>BOD₅ Removed (mg/L)</td>
<td>162</td>
<td>136</td>
<td>164</td>
<td>184</td>
</tr>
<tr>
<td>Average BOD₅ total (kg)</td>
<td>80.3</td>
<td>78.4</td>
<td>81</td>
<td>92.9</td>
</tr>
<tr>
<td>Average CO₂ off (kg/day)</td>
<td>118</td>
<td>115</td>
<td>119</td>
<td>136</td>
</tr>
<tr>
<td>Average CO₂ off (kg/year)</td>
<td>43,100</td>
<td>42,000</td>
<td>43,400</td>
<td>49,700</td>
</tr>
</tbody>
</table>


3.1.3.3 Power Demand

The power demand at Shelburne-Buckland includes two main processes: pumping and aeration. Pumping can be divided into two purposes, transporting the sewage to the plant and recirculating or transferring fluids from one point to another within the facility. The power demand for aeration is driven by the three blowers found in the aeration tank and the digester. Both blowers are fine bubble diffused aeration technology.

The Shelburne-Buckland Wastewater Treatment Facility reported using 167,000 kWh in 2015. Using the CO₂ output conversion rate, (EPA 2014), it is estimated that 115 metric tons of carbon dioxide was produced in 2015 from SBWWTP. Table 10 shows the estimated CO₂ produced from 2012-2015 due to power use.

\[ 6.89551 \times 10^{-4} \text{ metric tons } \text{CO}_2 / \text{kWh} \quad \text{(EPA 2014)} \]

\[ 167,000 \text{ kWh} \times 6.89551 \times 10^{-4} \text{ metric tons } \text{CO}_2 / \text{kWh} = 115 \text{ metric tons } \text{CO}_2 \text{ in 2015} \]
Table 10. AVERAGE DAILY FLOW, KWH USAGE, AND ESTIMATED CO₂ PRODUCED

<table>
<thead>
<tr>
<th>Year</th>
<th>2012</th>
<th>2013</th>
<th>2014</th>
<th>2015</th>
</tr>
</thead>
<tbody>
<tr>
<td>Average Flow (MGD)</td>
<td>0.131</td>
<td>0.152</td>
<td>0.160</td>
<td>0.133</td>
</tr>
<tr>
<td>Annual Usage kWh</td>
<td>164,000</td>
<td>154,000</td>
<td>170,000</td>
<td>166,000</td>
</tr>
<tr>
<td>kWh/MG</td>
<td>1,250,000</td>
<td>1,010,000</td>
<td>1,060,000</td>
<td>1,250,000</td>
</tr>
<tr>
<td>Total Annual Metric tons of CO₂</td>
<td>113</td>
<td>106</td>
<td>117</td>
<td>115</td>
</tr>
</tbody>
</table>

Provided data 2012-2015. Calculated annual metric tons of CO₂ produced from power demand.

3.1.3.4 Reed Bed Sludge Treatment

The greatest difference with Shelburne-Buckland Wastewater Treatment Plant as a conventional system is the use of Reed Bed Technology for onsite sludge processing. At the facility, the Reed Beds dewater, compost, and store the sludge for over 15 years. Dewatering efficiencies from 1992-1995 were calculated to be 96.9% (J.S. Begg et al. 2001). The Reed Beds provide on-site treatment of sludge, a higher volume and water reduction, and no power requirements for the treatment in the Red Beds. Additional benefits are the products of photosynthesis from the growth of the highly productive Phragmites. The total above and below ground primary productivity (TPP) for Phragmites australis was documented between 3.7 kg/m²/year and 9.39 kg/m²/year (Kadlec and Wallace 2008). Using the reverse of equation [7], we can calculate the approximate values of annual CO₂ used in photosynthesis by the Shelburne-Buckland Reed Beds.
TPP Phragmites = 3.7 kg/m²/year

Total Reed Bed area = 12,000 ft² = 1,111 m²

Total Plant Biomass = 4,100 kg/year

Using the reverse of equation [7] we can stoichiometrically calculate the CO₂.

\[
264 \text{kg CO}_2 + 108 \text{kg H}_2\text{O} \leftrightarrow 180 \text{kg C}_6\text{H}_{12}\text{O}_6 + 192 \text{kg O}_2 \quad [7]
\]

Estimated \( \text{CO}_2 = 6,027 \text{ kg/year} \)

3.1.4 Zumtobel Staff Lighting Vegetated Sand Beds Lloyd, NY

3.1.4.1 Biochemical Oxygen Demand

The average flow from Zumtobel Staff Lighting is 1,200 gallons per day or 0.0012 MGD. In 2007, the influent BOD₅ was 287 mg/L and the effluent was below 4 mg/L, resulting in a 99% removal rate.

Table 11 provides values for average daily flow, influent BOD₅, and effluent BOD₅ from 2001-2007 at Lloyd VSB.

Table 11. AVERAGE DAILY FLOW, INFLUENT BOD₅, AND EFFLUENT BOD₅

<table>
<thead>
<tr>
<th>Lloyd VSB</th>
<th></th>
<th></th>
<th></th>
<th></th>
<th></th>
<th></th>
<th></th>
</tr>
</thead>
<tbody>
<tr>
<td>Year</td>
<td>2001</td>
<td>2002</td>
<td>2003</td>
<td>2004</td>
<td>2005</td>
<td>2006</td>
<td>2007</td>
</tr>
<tr>
<td>Average Flow (MG)</td>
<td>0.0012</td>
<td>0.0012</td>
<td>0.0012</td>
<td>0.0012</td>
<td>0.0012</td>
<td>0.0012</td>
<td>0.0012</td>
</tr>
<tr>
<td>Influent BOD₅ (mg/L)</td>
<td>289</td>
<td>323</td>
<td>357</td>
<td>310</td>
<td>300</td>
<td>285</td>
<td>287</td>
</tr>
<tr>
<td>Effluent BOD₅ (mg/L)</td>
<td>5.14</td>
<td>6</td>
<td>&lt;4</td>
<td>&lt;4</td>
<td>&lt;4</td>
<td>&lt;4</td>
<td>&lt;4</td>
</tr>
</tbody>
</table>

Provided flow, influent BOD₅, and effluent BOD₅ from Lloyd VSB (Lavigne and Spokas 2008)
Figure 15 presents the influent and effluent BOD$_5$ values at Lloyd VSB from 2001-2007. The fluctuation of influent and effluent BOD$_5$ can easily be compared along with the change in BOD$_5$ removal.

![Lloyd VSB BOD$_5$ Removal](image)

Figure 15. AVERAGE INFLUENT AND EFFLUENT BOD$_5$ LLOYD VSB 2001-2007
Provided influent and effluent BOD$_5$ from 2001-2007 at Lloyd VSB (Lavigne and Spokas 2008).
3.1.4.2 Carbon Dioxide

The Carbon dioxide produced by the Lloyd Vegetated Sand Beds was calculated from the average BOD₅ removal and the average daily flow. Table 12 shows the CO₂ produced 2001-2007.

In 2007, the average influent BOD₅ was 287mg/L and effluent BOD₅ left at 4mg/L

\[ \text{BOD}_5 \text{ removed} = 283 \text{ mg/L} = 0.283 \text{kg/m}^3 \]

\[ 0.283 \frac{\text{kg}}{\text{m}^3} \cdot \frac{1 \text{ m}^3}{264 \text{ gal}} = 1.07 \times 10^{-3} \text{ kg of BOD}_5 \text{ per gallon} \]

Average Flow of 1,200 gallons per day

\[ 1,200 \frac{\text{gallons}}{\text{day}} \cdot 1.07 \times 10^{-3} \frac{\text{kg BOD}_5}{\text{gallon}} = 1.29 \text{ kg BOD}_5 \text{ per day} \]

Using equation [7], CO₂ emissions from microbial respiration, 1.47 kg of CO₂ is produced for every 1 kg of C₆H₁₂O₆, (represented by BOD₅).

\[ 180\text{kg C}_6\text{H}_{12}\text{O}_6 + 192\text{kg O}_2 \leftrightarrow 264\text{kg CO}_2 + 108\text{kg H}_2\text{O} \quad [7] \]

\[ 1.29 \text{ kg BOD}_5 / \text{day} \times 1.47 \text{kg CO}_2 / 1 \text{ kg BOD}_5 \]

Estimated CO₂ production from microbial respiration is 1.89 kg/day or 690 kg/year.

<table>
<thead>
<tr>
<th>Lloyd VSB</th>
<th>2001</th>
<th>2002</th>
<th>2003</th>
<th>2004</th>
<th>2005</th>
<th>2006</th>
<th>2007</th>
</tr>
</thead>
<tbody>
<tr>
<td>Year</td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Average Flow (MG)</td>
<td>0.0012</td>
<td>0.0012</td>
<td>0.0012</td>
<td>0.0012</td>
<td>0.0012</td>
<td>0.0012</td>
<td>0.0012</td>
</tr>
<tr>
<td>BOD₅ Removed (mg/L)</td>
<td>284</td>
<td>317</td>
<td>353</td>
<td>306</td>
<td>296</td>
<td>281</td>
<td>283</td>
</tr>
<tr>
<td>Average BOD₅ total (kg)</td>
<td>1.29</td>
<td>1.44</td>
<td>1.60</td>
<td>1.39</td>
<td>1.35</td>
<td>1.23</td>
<td>1.29</td>
</tr>
<tr>
<td>Average CO₂ off (kg/day)</td>
<td>1.90</td>
<td>2.12</td>
<td>2.36</td>
<td>2.04</td>
<td>1.98</td>
<td>1.88</td>
<td>1.89</td>
</tr>
<tr>
<td>Average CO₂ off (kg/year)</td>
<td>692</td>
<td>773</td>
<td>861</td>
<td>746</td>
<td>722</td>
<td>685</td>
<td>690</td>
</tr>
</tbody>
</table>

Table 12. AVERAGE BOD₅ REMOVAL AND ESTIMATED CO₂ PRODUCED

3.1.4.3 Photosynthesis

The benefit of CO$_2$ uptake from photosynthesis is calculated using the documented total primary productivity (TPP) of *Phragmites australis* and *Phalaris arundinacea* of 3.7kg/m$^2$/year (Kadlec and Wallace, 2008), and 2.03kg/m$^2$/year respectively, (Lyons, 2005).

Bed Area 1+2 with *Phalaris arundinacea* = 463 m$^2$ (2.028kg/m$^2$/year) = 939kg/ year

Bed Area 3+4 with *Phragmites australis* = 463 m$^2$ (3.7kg/m$^2$/year) = 1,713 kg/year

Total Plant Biomass = 2,650 kg/ year

Using the reverse of equation [7] we can stoichiometrically calculate the CO$_2$ used in photosynthesis.

$$264\text{kg CO}_2 + 108\text{kg H}_2\text{O} \leftrightarrow 180\text{kg C}_6\text{H}_{12}\text{O}_6 + 192\text{kg O}_2 [7]$$

$$2,650 \text{ kg biomass / year} \times 1.47\text{kg CO}_2/1 \text{ kg biomass}$$

Estimated CO$_2$ = $3,900 \text{ kg/year}$
3.1.5 Shushufindi Slaughterhouse VSBs, Ecuador, S. A.

3.1.5.1 Biochemical Oxygen Demand

The design flow from the Shushufindi slaughterhouse Vegetated Sand Beds is 25 m$^3$/day. The influent BOD$_5$ was recorded at 288 mg/L and the effluent left at 3mg/L, resulting in a 99% removal rate, in 2000. Table 13 presents values for average flow, influent BOD$_5$, and effluent BOD$_5$ per day from 1999-2000 at the Shushufindi slaughterhouse VSB.

Table 13. AVERAGE DAILY FLOW, INFLUENT BOD$_5$, AND EFFLUENT BOD$_5$

<table>
<thead>
<tr>
<th>Shushufindi Slaughterhouse VSB</th>
<th></th>
<th></th>
</tr>
</thead>
<tbody>
<tr>
<td>Year</td>
<td>1999</td>
<td>2000</td>
</tr>
<tr>
<td>Design Flow (m$^3$/day)</td>
<td>25</td>
<td>25</td>
</tr>
<tr>
<td>Influent BOD$_5$ (mg/L)</td>
<td>185</td>
<td>288</td>
</tr>
<tr>
<td>Effluent BOD$_5$ (mg/L)</td>
<td>5</td>
<td>3</td>
</tr>
</tbody>
</table>

Provided flow, influent BOD$_5$, and effluent BOD$_5$ from the Shushufindi slaughterhouse VSB (Kahl 2004).

Figure 16 provides the influent and effluent BOD$_5$ values at the Shushufindi slaughterhouse VSB from 1999-2000. The increase of influent BOD$_5$ and effluent BOD$_5$ can easily be compared along with the change in BOD$_5$ respired.
Figure 16. AVERAGE INFLUENT AND EFFlUENT BOD$_5$ AT SHUSHUFINDI SLAUGHTERHOUSE VSB

Provided influent and effluent BOD$_5$ from 2001-2007 at the Shushufindi slaughterhouse VSB (Kahl 2004).
3.1.5.2 Carbon Dioxide

The Carbon dioxide produced by the Shushufindi slaughterhouse VSBs was calculated from the average BOD₅ removal and the average daily flow. Table 14 shows the CO₂ produced in 1999 and 2001.

In 2000, the average influent BOD₅ was 288mg/L and effluent BOD₅ was 3mg/L.

\[
\text{BOD}_5 \text{ removed} = 285 \text{ mg/L} = 0.285 \text{ kg/m}^3
\]

Average Flow of 25m³/day

\[
\frac{25 \text{ m}^3}{\text{day}} \cdot 0.285 \frac{\text{kg BOD}_5}{\text{m}^3} = 7.13 \text{ kg BOD}_5 \text{ per day}
\]

Using equation [7], CO₂ emissions from microbial respiration, 1.47 kg of CO₂ is produced for every 1 kg of C₆H₁₂O₆, (represented by BOD₅).

\[
180 \text{ kg C}_6\text{H}_{12}\text{O}_6 + 192 \text{ kg O}_2 \leftrightarrow 264 \text{ kg CO}_2 + 108 \text{ kg H}_2\text{O} \quad [7]
\]

\[
7.13 \text{ kg BOD}_5/\text{day} \times 1.47 \text{ kg CO}_2/1 \text{ kg BOD}_5
\]

Estimated CO₂ production from microbial respiration is 10.5 kg/day or 3,820 kg/year.

Table 14. AVERAGE BOD₅ REMOVAL AND ESTIMATED CO₂ PRODUCED

<table>
<thead>
<tr>
<th>Shushufindi Slaughterhouse VSB</th>
<th>1999</th>
<th>2000</th>
</tr>
</thead>
<tbody>
<tr>
<td>Year</td>
<td></td>
<td></td>
</tr>
<tr>
<td>Design Flow (m³/day)</td>
<td>25</td>
<td>25</td>
</tr>
<tr>
<td>BOD₅ Removed (mg/L)</td>
<td>180</td>
<td>285</td>
</tr>
<tr>
<td>Average BOD₅ total (kg)</td>
<td>4.5</td>
<td>7.13</td>
</tr>
<tr>
<td><strong>Average CO₂ off (kg/day)</strong></td>
<td>6.62</td>
<td>10.5</td>
</tr>
<tr>
<td><strong>Average CO₂ off (kg/year)</strong></td>
<td>2,410</td>
<td>3,820</td>
</tr>
</tbody>
</table>

Provided flow and BOD₅ removal from Shushufindi Slaughterhouse VSB (Kahl 2004).
3.1.5.3 Photosynthesis

The benefit from CO$_2$ uptake during photosynthesis is calculated using the documented total primary productivity of German Grass, scientifically *Echinochloa polystachya* of 4kg/m$^2$/year (Kahl 2004).

Total VSB Area = 775 m$^2$ · (4kg/m$^2$/year) = 3,100 kg/year

Using the reverse of equation [7] we can stoichiometrically calculate the CO$_2$ used in photosynthesis.

$$264\text{kg CO}_2 + 108\text{kg H}_2\text{O} \leftrightarrow 180\text{kg C}_6\text{H}_{12}\text{O}_6 + 192\text{kg O}_2 \quad [7]$$

3,100 kg biomass / year x 1.47kg CO$_2$/ 1 kg biomass

Estimate CO$_2$ = 4,560 kg/year
3.1.6 Shushufindi Municipal VSBs Ecuador, S.A.

3.1.6.1 Biochemical Oxygen Demand

The design flow from Shushufindi Municipal Vegetated Sand Beds is 2,000 m³/day. The influent BOD₅ was recorded at 288mg/L and the effluent left at 1 mg/L, resulting in a 99% removal rate, in 2000.

Table 15 gives the values for average daily flow, influent BOD₅, and effluent BOD₅ from 1999-2000 at the Shushufindi municipal VSB.

Table 15. AVERAGE DAILY FLOW, INFLUENT BOD₅, AND EFFlUENT BOD₅

<table>
<thead>
<tr>
<th>Shushufindi Municipal VSB</th>
<th>1999</th>
<th>2000</th>
</tr>
</thead>
<tbody>
<tr>
<td>Design Flow (m³/day)</td>
<td>2,000</td>
<td>2,000</td>
</tr>
<tr>
<td>Influent BOD₅ (mg/L)</td>
<td>185</td>
<td>288</td>
</tr>
<tr>
<td>Effluent BOD₅ (mg/L)</td>
<td>5</td>
<td>1</td>
</tr>
</tbody>
</table>

Provided flow, influent BOD₅, and effluent BOD₅ from Shushufindi Municipal VSB (Kahl 2004).

Figure 17 shows the influent and effluent BOD₅ values at the Shushufindi Municipal VSB from 1999-2000. The increase of influent and effluent BOD₅ can easily be compared along with the change in BOD₅ removed.
Figure 17. AVERAGE INFLUENT BOD$_5$ AND EFFLUENT BOD$_5$ AT SHUSHUFINDI MUNICIPAL VSB
Provided influent and effluent BOD$_5$ from 1999-2000 at Shushufindi Municipal VSB (Kahl 2004).

3.1.6.2 Carbon Dioxide

The Carbon dioxide produced by the Shushufindi Municipal Vegetated Sand Beds was calculated from the average BOD$_5$ removal and the average daily flow.

In 2000, the average influent BOD$_5$ was 288mg/L and effluent BOD$_5$ was 1mg/L

\[
\text{BOD}_5 \text{ removed} = 287 \text{ mg/L} = 0.287 \text{ kg/m}^3
\]

Average Flow of 2,000m$^3$/day

\[
2,000 \text{ m}^3/\text{day} \cdot 0.287 \frac{\text{kgBOD}_5}{\text{m}^3} = 574 \text{ kg BOD}_5 \text{ per day}
\]

Using equation [7], CO$_2$ emissions from microbial respiration, 1.47 kg of CO$_2$ is produced for every 1 kg of C$_6$H$_{12}$O$_6$, (represented by BOD$_5$).
\[ 180\text{kg } C_6H_{12}O_6 + 192\text{kg } O_2 \leftrightarrow 264\text{kg } CO_2 + 108\text{kg } H_2O \quad [7] \]

\[ 574 \text{ kg BOD}_5 /\text{day} \times 1.47\text{kg } CO_2/ \text{1 kg } BOD_5 \]

Estimated CO\(_2\) production from microbial respiration is \textbf{844 kg/ day} or \textbf{308,100 kg/year}.

Table 16 presents the estimated CO\(_2\) produced in 1999 and 2000 Municipal VSBs.

\begin{table}[h]
\begin{tabular}{|c|c|c|}
\hline
\textbf{Shushufindi Municipal VSB} & \textbf{1999} & \textbf{2000} \\
\hline
Year & & \\
\hline
Design Flow (m\(^3\)/day) & 2,000 & 2,000 \\
BOD\(_5\) Removed (mg/L) & 180 & 287 \\
Average BOD\(_5\) total (kg) & 360 & 574 \\
Average CO\(_2\) off (kg/day) & 529 & 844 \\
Average CO\(_2\) off (kg/year) & 193,000 & 308,100 \\
\hline
\end{tabular}
\end{table}

Provided flow and BOD\(_5\) removal from Shushufindi Municipal VSB (Kahl 2004).

\subsection{3.1.6.3 Photosynthesis}

The benefit of CO\(_2\) uptake from photosynthesis is calculated using the documented total primary productivity of German Grass, scientifically \textit{Echinochloa polystachya} of 4kg/m\(^2\)/year (Kahl 2004).

Total VSB Area = 16,300 m\(^2\) \cdot (4kg/m\(^2\)/year) = 65,200 kg/year

Using the reverse of equation [7] we can stoichiometrically calculate the CO\(_2\) used in photosynthesis.

\[ 264\text{kg } CO_2 + 108\text{kg } H_2O \leftrightarrow 180\text{kg } C_6H_{12}O_6 + 192\text{kg } O_2 \quad [7] \]

\[ 65,200 \text{ kg biomass / year} \times 1.47\text{kg } CO_2/ \text{1 kg biomass} \]

Estimated CO\(_2\) = \textbf{95,800 kg/year}
3.2 Estimated Reduction of CO₂ with Hypothetical Reed Bed Treatment

Sludge processing at Amherst and Ithaca represent two typical conventional methods for sludge management: Gravity Belt Thickener to an Incinerator and Belt Filter Press to a landfill. Two hypothetical Reed Bed systems will be sized using the sludge production values from each facility. The land area necessary for treatment and the reduction of carbon dioxide production will be estimated.

3.2.1 Amherst Wastewater Treatment Plant, MA

3.2.1.1 Land Area Needed

The recommended loading rate for Reed Bed technology is 55 gallons sludge/ ft²/ year with 26 applications, (M. Watson 2002). Amherst transports approximately 5 million gallons of sludge per year.

\[
\text{Estimated Total Area} = \frac{\text{5,000,000 gallons}}{\text{year}} \div \frac{\text{55 gallons}}{\text{ft}^2 \cdot \text{year}^{-1}} = 90,900 \text{ft}^2 \text{ or } 8,440 \text{ m}^2
\]
3.2.1.2 Annual Carbon Dioxide Reduction

Using the total land area of 8,440 m², the known total above and below ground primary productivity for *Phragmites australis* documented as 3,700g/m²/year with (Kadlec and Wallace, 2008), and the reverse of equation [7], we can calculate the approximate CO₂ values.

\[
\text{TPP} \, \text{*Phragmites australis*} = 3.7 \, \text{kg/m}^2/\text{year}
\]

Total Reed Bed area= 8,440 m²

Total Plant Biomass

\[
(3.7 \, \text{kg/m}^2/\text{year}) \times (8,440 \, \text{m}^2) = 31,200 \, \text{kg Plant Biomass/ year}
\]

Using the reverse of equation [7] we can stoichiometrically calculate the CO₂ sequestered.

\[
264\text{kg CO}_2 + 108\text{kg H}_2\text{O} \leftrightarrow 180\text{kg C}_6\text{H}_{12}\text{O}_6 + 192\text{kg O}_2 \quad [7]
\]

\[
31,200 \, \text{kg biomass / year} \times 1.47\text{kg CO}_2/ \, 1 \, \text{kg biomass}
\]

Estimated CO₂ sequestered = **45,900 kg/year** or **45.9 metric tons of CO₂**

Current Sludge Management = 578 metric tons of CO₂

Estimated CO₂ sequestered using Reed Bed technology= - 45.9 metric tons of CO₂

Estimated Net Change = -624 metric tons of CO₂ per year

Figure 18 presents the estimated metric tons of CO₂ produced from conventional technology at Amherst from sludge transport and incineration from 2013-2015. The estimated net reduction of CO₂ produced when replacing conventional sludge management with the hypothetical Reed Bed technology is also included.
Figure 18. ANNUAL CO₂ PRODUCTION USING CONVENTIONAL AND RB TECHNOLOGIES AT AMHERST
Estimated metric tons of CO₂ produced by conventional sludge treatment and Reed Bed treatment for Amherst WWTP.

### 3.2.2 Ithaca Area Wastewater Treatment Facility, NY

#### 3.2.2.1 Land Area Needed

Ithaca pumps approximately 65.7 million gallons of sludge per year to the gravity belt thickeners.

\[
\text{Estimated Total Area} = \frac{65,700,000 \text{ gallons}}{\text{year}} \div \frac{55 \text{ gallons}}{ft^2 \cdot \text{year}^{-1}} = 1,190,000 \text{ ft}^2 \text{ or } 111,000 \text{ m}^2
\]
3.2.2.2 Annual Carbon Dioxide Reduction

Using the total land area of 111,000 m², the known total above and below ground primary productivity for *Phragmites australis* documented as 3.7 kg/m²/year (Kadlec and Wallace 2008), and the reverse of equation [7], we can calculate the approximate CO₂ values.

TPP Phragmites = 3.7 kg/m²/year

Total Reed Bed area = 111,000 m²

Total Plant Biomass = 411,000 kg/year

Using the reverse of equation [7] we can stoichiometrically calculate the CO₂ used in photosynthesis.

\[ 264\text{kg CO}_2 + 108\text{kg }\text{H}_2\text{O} \leftrightarrow 180\text{kg }\text{C}_6\text{H}_{12}\text{O}_6 + 192\text{kg O}_2 \]  

\[ 411,000 \text{kg biomass/year} \times 1.47 \text{kg CO}_2/\text{1 kg biomass} \]

Estimated CO₂ = 604,000 kg/year or 604 metric tons of CO₂

Current Sludge Management = 317 metric tons of CO₂

Estimated CO₂ sequestered using Reed Bed technology = -604 metric tons of CO₂

Net Production = -921 metric tons of CO₂ per year

Figure 19 illustrates the distribution of annual CO₂ produced from conventional sludge management at Ithaca for 2002-2003. The estimated net CO₂ uptake from photosynthesis in the hypothetical Reed Beds is also included.
Figure 19 shows estimated metric tons of CO₂ produced by conventional sludge treatment and Reed Bed treatment for Ithaca. The sludge leaving the Ithaca is about 22% solids and is trucked to a landfill. After treatment in the Reed Beds, the sludge is about 99% solids and requires minimal maintenance. Depending on the design and depth of Reed Beds, the accumulated sludge may not need removal for 15+ years.
3.3 Estimated Reduction of CO₂ with Hypothetical VSB Technology

Applying the kinetics equations of Vegetated Sand Bed technology, we can estimate the necessary land area for equal treatment. Using equation [4] and [5], the treatment time and the total area can be calculated.

\[ t = \frac{1}{k} \ln \left( \frac{C_0}{C_t} \right) \]  \hspace{1cm} [4]

Where \( C_0 \) = Average initial concentration of BOD (mg/L)
\( C_t \) = Average concentration of BOD at time \( t \) (mg/L)
\( k \) = 1.2 day\(^{-1}\)

\[ Q = \frac{A \cdot h \cdot f}{t} \]  \hspace{1cm} [5]

Where \( Q \) = Average daily flow rate
\( t \) = Treatment time in days
\( A \) = Wetland area
\( h \) = Wetland depth, assumed 0.61m
\( f \) = Porosity of media (.35)

3.3.1 Amherst Wastewater Treatment Plant, MA

The Amherst Wastewater Treatment Plant receives wastewater pumped from Amherst, North Amherst, and the University of Massachusetts with an average daily flow is 3.85 MGD in 2015. Using the total MGD the estimated necessary land area for Vegetated Sand Bed technology can be calculated.
3.3.1.1 Land Area Needed

Known Values:

\[ C_0 = 227 \text{ mg/L} \]
\[ C_t = 2 \text{ mg/L} \]
\[ k = 1.2 \text{ day}^{-1} \]

\[ t = \frac{1}{1.2 \cdot \text{day}^{-1}} \ln \left( \frac{227 \text{ mg/L}}{2 \text{ mg/L}} \right) \quad [4] \]

\[ t = 3.9 \text{ days} \]

Known Values:

\[ Q_{\text{total}} = 3.85 \text{ MGD or } 13,300 \text{ m}^3/\text{day} \]
\[ h = 0.61 \text{ m} \]
\[ f = 0.35 \]
\[ t = 3.0 \text{ days} \]

\[ 13,300 \text{ m}^3/\text{day} = \frac{A \cdot (0.61 \text{ m}) \cdot (0.35)}{3.9 \text{ days}} \quad [5] \]

VSB Area Amherst = 243,000 m³

3.3.1.2 Annual Carbon Dioxide Reduction

Using the total land area of 243,000 m², the known total primary productivity (TPP) for *Phalaris arundinecea*, Reed Canary Grass documented as 2.03kg/m²/year (Lyons, 2005), and using the reverse of equation [7], we can calculate the approximate CO₂ values.
TPP Reed Canary Grass = 2.03 kg/m²/year

Total Vegetated Sand Bed area = 243,000 m²

Total VSB Plant Biomass = 493,000 kg/year

Using the reverse of equation [7] we can stoichiometrically calculate the CO₂.

\[ 264 \text{ kg CO}_2 + 108 \text{ kg H}_2\text{O} \leftrightarrow 180 \text{ kg C}_6\text{H}_12\text{O}_6 + 192 \text{ kg O}_2 \quad [7] \]

\[ 493,000 \text{ kg biomass/year} \times 1.47\text{ kg CO}_2/\text{1 kg biomass} \]

CO₂ sequestered = 725,000 kg/year or 725 metric tons of CO₂/year

Average Power Demand for Treatment = 1,030 metric tons of CO₂/year

Estimated CO₂ sequestered with Vegetated Sand Bed = -725 metric tons of CO₂/year

Net Change with VSB Technology = -1,760 metric tons of CO₂/year produced

Figure 20 illustrates the proportion of CO₂ produced from BOD₅ microbial respiration and power demand at the current conventional WWTP. The entire treatment process currently produces approximately 3,210 metric tons of CO₂ annually. Figure 20 also includes the estimated CO₂ production when treating with the hypothetical Vegetated Sand Beds and Reed Beds. The estimated reduction of CO₂ produced when replacing conventional methods with VSB and RB technology was 74.4%. 
Figure 20. **ANNUAL CO₂ PRODUCTION: CONVENTIONAL VS. VSB AND RB TECHNOLOGIES AT AMHERST**

Estimated CO₂ production from current conventional Amherst WWTP in 2015 and estimated carbon dioxide reduction with Vegetated Sand Bed and Reed Bed technology.

### 3.3.2 Ithaca Area Wastewater Treatment Plant, NY

The Ithaca Area Wastewater Treatment Plant receives wastewater an average 7.03 MGD pumped from Ithaca City. The average influent and effluent BOD₅ were 186 mg/L and 8.7 mg/L respectively. Using these values the estimated necessary land area for Vegetated Sand Bed technology can be calculated.
### 3.3.2.1 Land Area Needed

Known Values:

\[ C_0 = 186 \text{ mg/L} \]
\[ C_t = 8.7 \text{ mg/L} \]
\[ k = 1.2 \text{ day}^{-1} \]

\[
t = \frac{1}{1.2 \text{ day}^{-1}} \ln \left( \frac{186 \text{ mg/L}}{8.7 \text{ mg/L}} \right) \tag{4}
\]

\[ t = 2.55 \text{ days} \]

Known Values:

\[ Q_{\text{Total}} = 7.03 \text{ MGD or } 26,600 \text{ m}^3/\text{day} \]
\[ h = 0.61 \text{ m} \]
\[ f = 0.35 \]
\[ t = 2.55 \text{ days} \]

\[
26,600 \text{ m}^3/\text{day} = \frac{A \cdot (0.61 \text{ m}) \cdot (0.35)}{2.55 \text{ days}} \tag{5}
\]

VSB Area Total = 318,000 m²

### 3.3.2.2 Annual Carbon Dioxide Reduction

Using the total land area of 318,000 m², the known total primary productivity (TPP) for *Phalaris arundinecea*, Reed Canary Grass documented as 2.03 kg/m²/year respectively, (Lyons, 2005), and using the reverse of equation [7], we can calculate the approximate CO₂ values.
TPP Reed Canary Grass = 2.03 kg/m²/year

Total Vegetated Sand Bed area= 318,000 m²

Estimated Total Plant Biomass= 645,000 kg/ year

Using the reverse of equation [2] we can stoichiometrically calculate the CO₂.

\[
264\text{kg CO}_2 + 108\text{kg H}_2\text{O} \leftrightarrow 180\text{kg C}_6\text{H}_{12}\text{O}_6 + 192\text{kg O}_2
\]  

\[
645,000 \text{kg biomass / year} \times 1.47\text{kg CO}_2/1 \text{kg biomass}
\]

CO₂ sequestered = \textbf{948,000 kg/year} or \textbf{948 metric tons of CO₂}

Average Power Demand for Treatment = \textbf{2,850 metric tons of CO₂/year}

Estimated CO₂ sequestered with Vegetated Sand Bed = - \textbf{948 metric tons of CO₂/year}

Net Change with VSB = -\textbf{3800 metric tons of CO₂/year emitted}

Figure 21 presents the proportion of CO₂ produced from the BOD₅ microbial respiration and power demand at the conventional facility. The entire treatment process at Ithaca produced approximately 5,580 metric tons of CO₂ annually. Figure 21 also includes the estimated CO₂ production when treating with the hypothetical Vegetated Sand Beds and Reed Beds. The estimated reduction of CO₂ produced when replacing conventional methods with VSB and RB technology is 84.6%.
**Figure 21. ANNUAL CO₂ PRODUCTION: CONVENTIONAL VS. VSB AND RB TECHNOLOGY AT ITHACA**

Estimated CO₂ production from conventional Ithaca and estimated carbon dioxide reduction with Vegetated Sand Bed and Reed Bed technology.

### 3.3.3 Shelburne-Buckland Wastewater Treatment Plant, MA

Shelburne-Buckland Wastewater Treatment Plant uses activated sludge technology with aerobic sludge digestion. The facility processes on average 0.133MGD, with an average influent BOD₅ of 158 mg/L and an average effluent of 4.7 mg/L (Begg et al. 2001). Using these known values, the land area needed for VSB treatment can be estimated.
3.3.3.1 Land Area Needed

Known Values:

\[ C_0 = 158 \, \text{mg/L} \]
\[ C_t = 4.7 \, \text{mg/L} \]
\[ k = 1.2 \, \text{day}^{-1} \]

\[ t = \frac{1}{1.2 \cdot \text{day}^{-1}} \ln \left( \frac{158 \, \text{mg/L}}{4.7 \, \text{mg/L}} \right) \quad [5] \]

\[ t = 3.07 \, \text{days} \]

Known Values:

\[ Q_{\text{Total}} = 0.133 \, \text{MGD or 503 m}^3/\text{day} \]
\[ h = 0.61 \, \text{m} \]
\[ f = 0.35 \]

\[ t = 3.07 \, \text{days} \]

\[ 503 \, \text{m}^3/\text{day} = \frac{A \cdot (0.61 \, \text{m}) \cdot (0.35)}{3.07 \, \text{days}} \quad [6] \]

\[ \text{VSB Area Total} = 7,230 \, \text{m}^2 \]

3.3.3.2 Annual Carbon Dioxide Reduction

Using the total land area of \( 7,230 \, \text{m}^2 \), the known total primary productivity (TPP) for \textit{Phalaris arundineacea}, Reed Canary Grass documented as 2.03kg/m^2/year (Lyons 2005), and with the reverse of equation [7], we can calculate the approximate CO\(_2\) values.
TPP Reed Canary Grass = 2.03 kg/m²/year

Total Vegetated Sand Bed area= 7,230 m²

Total Plant Biomass= 14,700 kg/ year

Using the reverse of equation [2] we can stoichiometrically calculate the CO₂ sequestered.

\[ 264\text{kg CO}_2 + 108\text{kg H}_2\text{O} \leftrightarrow 180\text{kg C}_6\text{H}_{12}\text{O}_6 + 192\text{kg O}_2 \]  

\[ 14,700 \text{ kg biomass/ year} \times 1.47\text{kg CO}_2/1 \text{ kg biomass} \]

Estimated CO₂ sequestered = **21,600 kg/year or 21.6 metric tons of CO₂/year**

Average Power Demand for Secondary Treatment = **115 metric tons of CO₂/year**

Estimated CO₂ sequestered with Vegetated Sand Bed = - **21.6 metric tons of CO₂/year**

Net Change = -**137 metric tons of CO₂/year produced**

Figure 22 presents the total carbon dioxide produced from current conventional treatment at Shelburne-Buckland. The entire conventional treatment process with RB sludge processing produced approximately 159 metric tons of CO₂ annually. Figure 22 also includes the estimated net CO₂ production using the hypothetical Vegetated Sand Beds for treatment. The estimated reduction of CO₂ produced when replacing conventional methods with VSB technology is 86.2%.
Figure 22. **ANNUAL CO₂ PRODUCTION: CONVENTIONAL VS. VSB AND RB TECHNOLOGY AT SHELBURNE-BUCKLAND**

Estimated CO₂ production from Shelburne-Buckland WWTP in 2015, with projected reduction when using Vegetated Sand Bed technology.
CHAPTER 4
DISCUSSION

This study investigates the sustainability of conventional wastewater treatment compared to Vegetated Sand Bed and Reed Bed technology with focus on CO$_2$ production. The three main sources of CO$_2$ production considered were BOD$_5$ microbial respiration, power demand, and sludge processing. The production of CO$_2$ from each source was estimated and totaled for each facility allowing for the comparison between individual processes and treatment technology as a whole.

4.1 Conventional Treatment Efficiency

When comparing the total metric tons of CO$_2$ produced per million gallons of wastewater treated, it is important to consider the average daily flow of the facility. As shown in the collaboration of *Electricity Use and Management in the Municipal Water Supply and Wastewater Industries* report from 2013, electricity use per MG increase greatly as the average daily flow of the facility decreases. Figure 23 illustrates the relationship between energy demand and average plant flow in MGD. With conventional technology, facilities with the lowest average plant flow have the greatest electrical demand and total CO$_2$ production per MG of wastewater treatment. Electricity use in kWh/MG for hypothetical VSB and RB systems is also shown in Figure 23. The average electrical demand is estimated to be negligible and is not dependent on plant flow.
Figure 23. DAILY ELECTRICAL USE COMPARED TO AVERAGE PLANT FLOW IN MGD
Adapted from the Electricity Use and Management in the Municipal Water Supply and Wastewater Industries report from 2013, Figure 23 presents electricity compared to average plant flow. Electricity for hypothetical VSB and RB systems are also included showing the electricity use is not dependent on average facility flow.

4.2 Conventional Treatment Comparison

When comparing efficiency and CO₂ production between conventional facilities, it is necessary to understand the average daily flow. Shelburne-Buckland uses 1.25 million kWhrs per MG of wastewater treated producing 1,240 metric tons of CO₂ per MG. Ithaca uses 501,000 kWhrs per MG and only 899 Metric tons of CO₂ per MG. The total annual metric tons produced by each facility is 6,320 at Ithaca and only 159 metric tons of CO₂ from Shelburne-Buckland. Figure 24 presents the relationship of annual CO₂ produced to plant flow. The plant with the lowest average flow produces the highest metric tons of CO₂ per million gallons treated.
Figure 24. CO₂ PER MILLION GALLONS AT AMHERST, ITHACA, AND SHELBURNE-BUCKLAND
Data provided from Amherst, Ithaca, and Shelburne-Buckland used to estimate CO₂ produced.

Figure 25 shows the total annual metric tons of CO₂ at the three conventional facilities. When just looking at the total production, the annual CO₂ produced is a function of plant flow. Figure 25 does not address the CO₂/MG efficiency of the conventional facilities.
Figure 25. **ANNUAL CO\textsubscript{2} PRODUCED AT AMHERST, ITHACA, AND SHELBURNE-BUCKLAND**
Data provided from Amherst, Ithaca, and Shelburne-Buckland used to estimate CO\textsubscript{2} produced.

### 4.3 Annual CO\textsubscript{2} Produced: Conventional vs. VSB and RB Technology

The total metric tons of CO\textsubscript{2} produced from treatment at each conventional facility are broken down in Table 17. The power use for conventional treatment and treatment in the hypothetical VSB and RB systems are presented. The CO\textsubscript{2} uptake during photosynthesis in the VSB and RB systems are calculated. Using the values in Table 17 the net total CO\textsubscript{2} produced from VSB and RB treatment is estimated. Finally, the percent reduction of metric tons of CO\textsubscript{2} produced when converting conventional wastewater treatment to VSB and RB technology is calculated.
Table 17. TOTAL ANNUAL CO₂ PRODUCED FROM CONVENTIONAL FACILITIES

<table>
<thead>
<tr>
<th>Metric Tons of CO₂ Produced</th>
<th>Amherst</th>
<th>Ithaca</th>
<th>Shelburne-Buckland</th>
</tr>
</thead>
<tbody>
<tr>
<td>BOD₅ Microbial Respiration</td>
<td>1,590</td>
<td>2,410</td>
<td>44</td>
</tr>
<tr>
<td>Power Use Conventional</td>
<td>1,610</td>
<td>3,170</td>
<td>115</td>
</tr>
<tr>
<td>Power Use VSB and RB</td>
<td>0</td>
<td>0</td>
<td>0</td>
</tr>
<tr>
<td>Photosynthesis in VSB and RB</td>
<td>-771</td>
<td>-1,550</td>
<td>-22</td>
</tr>
<tr>
<td>Net Total with VSB and RB</td>
<td>819</td>
<td>858</td>
<td>22</td>
</tr>
<tr>
<td>Percent Reduction from Conventional</td>
<td>74.4</td>
<td>84.6</td>
<td>86.2</td>
</tr>
</tbody>
</table>

Estimated annual metric tons of CO₂ are compiled in Table 16. Values are calculated using provided data from each facility.

Figure 26 presents the current conventional power use production of metric tons of CO₂ and the estimated reduction with the use of VSB and RB technology. Unlike the conventional treatment, the power use with VSB and RB technology regardless of average daily flow, is zero. The CO₂ produced from BOD₅ microbial respiration is reduced with VSB and RB application due to the CO₂ uptake from photosynthesis. The reduction of CO₂ production from the Amherst, Ithaca, and Shelburne-Buckland are 74.4%, 84.6%, and 86.2% respectively.
Figure 26. ANNUAL CO₂ PRODUCED: COMPARISON OF CONVENTIONAL, VSB, AND RB TECHNOLOGY

Figure 26 shows the annual metric tons of CO₂ produced at Amherst, Shelburne-Buckland, Ithaca, Lloyd, Shushufindi Slaughterhouse, and Shushufindi Municipal. The hypothetical VSB and RB systems for Amherst, Shelburne-Buckland, and Ithaca are also included showing total net CO₂ produced. Data provided from Amherst, Ithaca, and Shelburne-Buckland used to estimate CO₂ produced using current conventional technology and hypothetical VSB and RB technology.

In Figure 27, the only CO₂ production at the Lloyd VSB, Shushufindi slaughterhouse VSB, and Shushufindi Municipal VSB, was from the BOD₅ microbial respiration in the systems. Due to the photosynthesis occurring in each VSB and RB system, the net CO₂ emission values were further reduced. The annual metric tons of CO₂ from Figure 27 are presented in Table 18 showing the reduced CO₂ production from wastewater treatment when converting conventional treatment to VSB and RB.
technology. The net CO$_2$ value for the Lloyd VSB and the Shushufindi Slaughterhouse VSB was estimated at -3.21 metric tons of CO$_2$ and -1.6 metric tons of CO$_2$ suggesting the possibility of CO$_2$ sequestering systems.

Figure 27. METRIC TONS OF CO$_2$ PRODUCED: APPLYING HYPOTHETICAL VSB AND RB TECHNOLOGY
Data provided from Amherst, Ithaca, and Shelburne-Buckland WWTP, Lloyd (Lavigne and Spokas 2008), Shushufindi Slaughterhouse (Kahl 2004), and Shushufindi Municipal, (Kahl 2004) used to estimate CO$_2$ produced.

Table 18. ANNUAL CO$_2$ PRODUCED: CONVENTIONAL VS. VEGETATED SAND BED AND REED BED TECHNOLOGY

<table>
<thead>
<tr>
<th>Annual Metric Tons of CO$_2$</th>
<th>Amherst</th>
<th>Shelburne-Buckland</th>
<th>Ithaca</th>
<th>Lloyd</th>
<th>Shush. Slaughterhouse</th>
<th>Shush. Municipal</th>
</tr>
</thead>
<tbody>
<tr>
<td>Conventional</td>
<td>3,210</td>
<td>159</td>
<td>5,580</td>
<td>N/A</td>
<td>N/A</td>
<td>N/A</td>
</tr>
<tr>
<td>VSB and RB</td>
<td>823</td>
<td>22</td>
<td>930</td>
<td>-3.21</td>
<td>-1.6</td>
<td>212</td>
</tr>
</tbody>
</table>
4.4 CO₂ Produced per Million Gallons: Conventional vs. VSB and RB Technology

Figure 28 illustrates the relationship between average daily flow and energy use per MG at conventional facilities. With the application of the hypothetical Vegetated Sand Bed and Reed Bed technology, the CO₂ production is greatly reduced and the size of the facility no longer independently determines the CO₂ per MG relationship.

![Metric Tons of CO₂ Produced per Million Gallons](image)

**Figure 28. CO₂ PRODUCED PER MGD: COMPARISON OF CONVENTIONAL TREATMENT VS. VEGETATED SAND BED AND REED BED TECHNOLOGY**

Estimated CO₂ production at conventional facilities compared to CO₂ production applying hypothetical VSB and RB technology. Data provided from Amherst, Ithaca, and Shelburne-Buckland used to estimate CO₂ produced.
CHAPTER 5
CONCLUSION

The objective of this research is to compare the sustainability of conventional wastewater treatment with Vegetated Sand Bed and Reed Bed technology considering the fate of fresh water, CO$_2$ production, and total energy consumption.

Vegetated Sand Bed and Reed Bed technologies are sustainable systems that could shift conventional treatment towards greener water management methods. Conventional wastewater treatment is the product of linear thinking and is not sustainable. In the United States, the anthropogenic water use cycle extracts fresh water from the environment and puts it through treatment. The treated water is contaminated or wasted and sent back to a treatment facility. The treated effluent is disinfected, often with chlorine, before it is discharged into a river ending up in the ocean. The United States needs to start managing water as a resource to recycle rather than waste of which to dispose. VSB and RB technology can be the shift in wastewater treatment to more sustainable methods. Using VSB and RB systems provides high quality treatment that can work without the high energy input required at most conventional wastewater facilities.

Greater than half the total CO$_2$ produced at conventional facilities was due to the power demand at every conventional facility. Table 19 shows the carbon dioxide produced from BOD$_5$ microbial respiration and power demand. The reduction or elimination of the power use from conventional treatment could decrease the total CO$_2$ produced by over 50%.
Table 19. TOTAL ANNUAL CO\textsubscript{2} PRODUCED AT CONVENTIONAL FACILITIES FROM POWER DEMAND

<table>
<thead>
<tr>
<th></th>
<th>Amherst</th>
<th>Shelburne-Buckland</th>
<th>Ithaca</th>
</tr>
</thead>
<tbody>
<tr>
<td>Average Flow (MGD)</td>
<td>3.51</td>
<td>0.133</td>
<td>7.03</td>
</tr>
<tr>
<td>BOD\textsubscript{5} Removal</td>
<td>1,510</td>
<td>44</td>
<td>2,410</td>
</tr>
<tr>
<td>Power Demand</td>
<td>1,610</td>
<td>115</td>
<td>3,170</td>
</tr>
<tr>
<td>Total Metric tons CO\textsubscript{2}</td>
<td>3,120</td>
<td>159</td>
<td>5,580</td>
</tr>
</tbody>
</table>

Data provided from Amherst, Ithaca, and Shelburne-Buckland used to estimate CO\textsubscript{2} produced.

Vegetated Sand Bed and Reed Bed technology can eliminate the power demand for sewage treatment, resulting in greater than 50% reduction of CO\textsubscript{2} produced. Additionally, the facultative wetland plants in each VSB and RB system photosynthesize further reducing the net CO\textsubscript{2} produced during wastewater treatment.

Figure 29 compiles the net annual CO\textsubscript{2} production from all conventional and VSB systems in this study. The sources of CO\textsubscript{2} are BOD\textsubscript{5} microbial respiration, power use, and photosynthesis.
Estimated CO\textsubscript{2} values from BOD\textsubscript{5} microbial respiration, power use, and photosynthesis for conventional, Amherst, Ithaca, Shelburne-Buckland and Vegetated Sand Bed treatment, Lloyd, Shushufindi Municipal, and the Shushufindi Slaughterhouse.

Figure 30 compares the change of CO\textsubscript{2} production per MG treated from conventional treatment to VSB and RB technology. This shows the CO\textsubscript{2} produced/MG at conventional facilities is dependent on the size of the facility. Smaller facilities produce much higher CO\textsubscript{2} which is due to higher power use/MG treated. Also shown on this graph is the CO\textsubscript{2} production from the hypothetical VSB and RB systems. The VSB and RB systems require no power and this is apparent on the graph. This graph suggests the efficiency of conventional treatment is dependent on the average flow of the facility. Also, when using VSB and RB technology in place of conventional, the efficiency will be greatly reduced and no longer dependent on the facility size.
Figure 30. **TOTAL METRIC TONS OF CO$_2$ PRODUCED PER AVERAGE PLANT FLOW IN MGD**

Data provided from Amherst, Ithaca, and Shelburne-Buckland used to estimate CO$_2$ produced from current conventional treatment and treatment using hypothetical VSB and RB technology.

One limitation of Vegetated Sand Beds many address is the physical limitations and high costs of land area. VSB and RB systems require more land area so they cannot simply replace established treatment facilities. Along with rethinking the approach on water management, typical methods can be challenged. VSB and RB systems fit in many undesirable plots of land. One example of an innovative location to implement VSB and RB technology would be an established wetland when no one can build. Many wetlands run along roads, farms, and industries receiving contaminates from non-point sources. Building VSBs and RBs in locations such as these could establish new green wastewater treatment facilities as well as improve the quality of water entering the environment; many places receive elevated levels of nutrients or contaminants due to non point source discharge. Many processes in Vegetated Sand Beds are not understood and present opportunities for further investigation.
CHAPTER 6

THE JOSEPH TROLL TURF RESEARCH CENTER- A CASE STUDY OF VSB’s USED TO TREAT COMPLEX ORGANICS AND NUTRIENTS

In 2011 the Golf Course Superintendents of America (GCSAA) financed an experimental VSB project to see if the technology can treat several of the chemicals used in golf course maintenance. They can generally be described as nutrients, herbicides, pesticides, and fungicides. With the permission of Dr. Ronald Lavigne owner of U.S. patent number 7,510,649; Lavigne, 2009, a four cell VSB was constructed and put online in the summer of 2015. Figure 31 illustrates the cross sectional view of the facility and Figure 32 shows the plan view.

Photo 10. West View Joseph Troll Turf Research Center VSBs

Photo 11. East View Joseph Troll Turf Research Center VSBs
Photo 12. South View Joseph Troll Turf Research Center VSBs

Figure 31. CROSS-SECTIONAL AREA OF JOSEPH TROLL TURF PLOT RESEARCH VSB
Nitrogen compounds are an increasing concern in wastewater and because of their role in eutrophication, their effect on oxygen levels on receiving waters, and their toxicity to vertebrate and invertebrate species, (Kadlec and Knight 1996). Ammonium is an inorganic compound that can greatly impact wetland environments when released into the environment. It is the preferred nutrient form of nitrogen for most wetland plants as well as for autotrophic bacteria. Ammonium is readily oxidized in natural waters resulting in significant O₂ consumption and it is also toxic to many forms of aquatic life at low concentrations (Kadlec and Knight 1996). An excess release of nitrate in wastewater can lead to eutrophication of surface waters because it is an essential nutrient for plant growth. It is also a concern
with water control because it is toxic to infants and linked to methylglobanemia (Kadlec and Knight 1996). The focus of the fate of ammonium and nitrate was spurred by the rising problem of nitrate in groundwater on Cape Cod where golf courses have been pressed to eliminate potential nitrogen runoff.

Early objectives were to:

I. Determine the hydraulic retention time of treatment within the system

II. Operate the facility in the “batch mode” with varying retention time to secure concentration vs. time data

III. See if the microbial reduction of organic and inorganic species would follow a first order decay model.

\[
\frac{dC}{dt} = -k \cdot C \tag{8}
\]

Where \( C \) is the concentration (mg/L)

\( t \) is treatment time (days)

\( k \) is first order decay rate constant (days\(^{-1}\))

\[
\ln C_t = -kt + \ln C_0 \tag{9}
\]

Where \( C_t \) is concentration at time \( t \) (mg/L)

\( C_0 \) is concentration at time zero (mg/L)

By late fall preliminary data had been assembled and by separating variables and integrating equation [8], a linear form of the first order decay model is \( \ln C = -kt + \ln C_0 \). The plot of that data is illustrated in figure 33. The slope of the plot indicates a rate constant of approximately 0.14 days\(^{-1}\) for ammonium removal with an average 72% reduction of NH\(_4^+\). A similar study conducted by L. A. Spokas, S. C. Simkins, P. L. Veneman, and S. C. Long investigated the performance of a constructed wetland removing NH\(_4^+\) and NO\(_3^-\) primary domestic wastewater effluent. In this study, the VSB PB1 had an
influent and effluent concentration of 30.4 ± 9.2 mg/L and 9.8 ± 7.9 mg/L with a mean ammonium rate constant of 0.13 ± 0.08, (Spokas et al. 2010). The Joseph Troll Turf Plot VSBs had an influent and effluent concentration of 26.43 mg/L and 6.19 mg/L of NH$_4^+$ shown in Figure 34.

Figure 33 shows promising preliminary results for ammonium reduction in a Vegetated Sand Bed. The reduction of ammonium suggests the VSB provides sufficient oxygen in the media to support nitrification. This also suggests the VSB has a population of nitrifiers in the system.
Figure 34. CHANGE IN AMMONIUM CONCENTRATION OVER TIME

Figure 35 presents the first order decay rate of \(0.23 \text{ days}^{-1}\) for \(\text{NO}_3^-\). Figure 36 shows the nitrate concentration reduction over the span of 12 days with an average 88% removal. The data presented in Figures 33-36 represent the removal of nitrate and ammonium in the fall and further investigation is needed to understand the seasonal variations.
Figure 35. FIRST ORDER NITRATE REDUCTION

Figure 35 shows promising preliminary results for the reduction of nitrate in a Vegetated Sand Bed. These results suggest the VSB system provides sufficient anaerobic zones to support denitrifying microorganisms. It is not known if the denitrifiers are heterotrophs or autotrophs, but the denitrification did not appear to be limited by insufficient carbon source. The effect of nitrification of ammonium occurring simultaneously was not accounted for and needs further investigation.
The removal of organic and inorganic nitrogen from wastewater before it is discharged is important for the future health of the environment and all who depend on it. The preliminary ammonium and nitrate removal testing at the Joseph Troll Turf Plot Research VSB suggest both can be removed with this technology. Further research can investigate the processes occurring in the VSB to provide the removal of the contaminant and the fate of the nitrogen. Testing the ammonium and nitrate separately will also give a better representation of the rate of removal as well as the concentration in the VSB.

Figure 36. CHANGE IN NITRATE CONCENTRATION OVER TIME

The removal of organic and inorganic nitrogen from wastewater before it is discharged is important for the future health of the environment and all who depend on it. The preliminary ammonium and nitrate removal testing at the Joseph Troll Turf Plot Research VSB suggest both can be removed with this technology. Further research can investigate the processes occurring in the VSB to provide the removal of the contaminant and the fate of the nitrogen. Testing the ammonium and nitrate separately will also give a better representation of the rate of removal as well as the concentration in the VSB.
In the spring and summer of 2016, the batch studies will be expanded to include more complex organics with the objective of refining a design model for multiple parameters. Construction of a full scale VS8 facility will begin during the summer of 2016 at the Yarmouth Massachusetts Bayberry Hill Country Club with design, construction supervision, and monitoring by UMASS and New England Waste Systems U.S.A. (NEWS-USA). It is expected that other golf courses around the country will employ the technology to protect the environment including ground and surface water resources.
LITERATURE CITED


